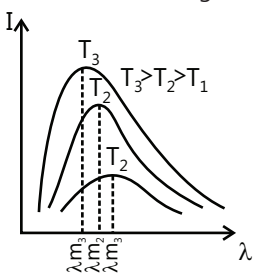


7.	Radiation	Every body radiates electromagnetic radiation of all possible wavelength at all temp > 0 K
8.	Stefan's Law	<p>Rate of heat emitted by a body at temp T K from per unit area <math>E = \sigma T^4</math> J / sec / m<sup>2</sup></p> <p>Radiation power <math>\frac{dQ}{dT} = P = \sigma AT^4</math> watt</p> <p>If body is placed in a surrounding of temperature <math>T_s</math> <math>\frac{dQ}{dT} = \sigma A(T^4 - T_s^4)</math> valid only for black body</p> <p>Emissivity or emmision power <math>e = \frac{\text{heat from general body}}{\text{heat from black body}}</math></p> <p>If temp of body falls by dT in time dt</p> <p><math>\frac{dT}{dt} = \frac{eA\sigma}{ms}(T^4 - T_s^4)</math> (dT/dt=Rate of cooling)</p>
9.	Newton's law of cooling	<p>If temp difference of body with surrounding is small i.e.</p> <p><math>T = T_s</math> Then, <math>\frac{dT}{dt} = \frac{4eA\sigma}{ms} T_s^3 (T - T_s)</math> So <math>\frac{dT}{dt} \propto (T - T_s)</math></p>
10.	Average form of Newton's law of cooling	<p>If a body cools from <math>T_1</math> to <math>T_2</math> in time <math>\delta t</math></p> <p><math>\frac{T_1 - T_2}{\delta t} = \frac{K}{mS} \left( \frac{T_1 + T_2}{2} - T_s \right)</math> (Used generally in objective questions) <math>\frac{dT}{dt} = \frac{K}{mS} (T - T_s)</math></p> <p>(For better results use this generally in subjective )</p>
11.	Wien's black body radiation	<p>At every temperature (&gt;0K) a body radiates energy radiations of all wavelengths. According to Wien's displacement law if the wavelength corresponding to maximum energy is <math>\lambda_m</math> then <math>\lambda_m T = b</math></p> <p>where b= is a constant( Wien's Constant )</p> <p>T=Temperature of body</p> 

## Solved Examples

### JEE Main/Boards

**Example 1:** A copper rod 2 m long has a circular cross section of radius 1 cm. One end is kept at 100°C and other at 0°C, and the surface is insulated so that negligible heat is lost through the surface. Find

(a) The thermal resistance of bar

(b) The thermal current H

(c) The temperature gradient  $\frac{dT}{dx}$

(d) The temperature 25 cm from hot end. Thermal conductivity of copper is 401 W/m-K

**Sol:** Recall the formula of heat transfer.

(a) Thermal resistance

$$R = \frac{1}{kA} = \frac{1}{k(\pi r^2)} \quad \text{or} \quad R = \frac{2}{(401)(\pi)(10^{-2})^2} = 15.9 \text{ K / W}$$

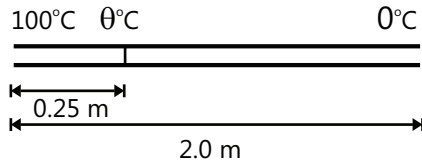
(b) Thermal current,  $H = \frac{\Delta T}{R} = \frac{\Delta \theta}{R} = \frac{100}{15.9}$  or

$$H = 6.3 \text{ W}$$

(c) Temperature gradient

$$= \frac{0 - 100}{2} = -50 \text{ K / m} = -50^\circ \text{C / m}$$

(d) Let be  $\theta^\circ\text{C}$  the temperature at 25 cm from hot end then



$$\begin{aligned} (\theta - 100) &= (\text{Temperature gradient}) \times (\text{Distance}) \\ \theta - 100 &= (-50)(0.25) \\ \theta &= 87.5^\circ\text{C} \end{aligned}$$

**Example 2:** In a murder investigation, a corpse was found by a detective at exactly 8 P.M. Being alert, the detective also measured the body temperature and found it to be  $70^\circ\text{F}$ . Two hours later, the detective measured the body temperature again and it found to be  $60^\circ\text{F}$ . If the room temperature is  $50^\circ\text{F}$ , and assuming that the body temperature of the person before death was  $98.6^\circ\text{F}$ , at what time did the murder occur?

**Sol:** Newton's law of cooling is used.

With time 0 taken to be 8 P.M., we have the boundary value problem

$$\frac{dT}{dt} = k(50 - T); \quad \begin{aligned} T(0) &= 70 \\ T(2) &= 60 \end{aligned}$$

Whose solution is  $T = 50 + 20\left(\frac{1}{2}\right)^{t/2}$

We would like to find the value of  $t$  for which  $T(t) = 98.6$ . Solving the equation

$$50 + 20\left(\frac{1}{2}\right)^{t/2} = 98.6$$

$$\text{Given us } t = 2\left(\frac{\ln(48.6/20)}{\ln(1/2)}\right) \approx -2.56.$$

It appears that this person was murdered at about 530 P.M. or so.

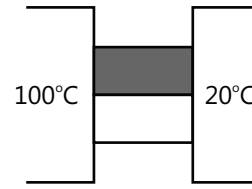
From the function  $T = 50 + 20\left(\frac{1}{2}\right)^{t/2}$

Over the time interval  $-2.56 \leq t \leq 2.56$ .

**Example 3:** Two metal cubes with 3 cm edges of copper and aluminium are arranged as shown in fig. find

- (a) The total thermal current from one reservoir to the other
- (b) The ratio of the thermal current carried by the copper cube to that of the aluminium cube. Thermal

conductivity of copper is  $401 \text{ W/m-K}$  and that of aluminium is  $237 \text{ W/m-K}$



**Sol:** This is parallel combination and thermal current would be sum of both cubes.

(a) Thermal resistance of aluminum cube

$$R_1 = \frac{1}{kA} \text{ or } R_1 = \frac{(3 \times 10^{-2})}{(237)(3 \times 10^{-2})^2} = 0.14 \text{ K/W}$$

and Thermal resistance of aluminum cube

$$R_2 = \frac{(3 \times 10^{-2})}{(401)(3 \times 10^{-2})^2} = 0.08 \text{ K/W}$$

As these two resistances are in parallel, their equivalent resistance will be

$$R = \frac{R_1 R_2}{R_1 + R_2} = \frac{(0.14)(0.08)}{(0.14) + (0.08)} = 0.05 \text{ K/W}$$

Thermal Current  $H = \frac{\text{Temperature difference}}{\text{Thermal resistance}}$

$$= \frac{(100 - 20)}{0.05} = 1.6 \times 10^3 \text{ W}$$

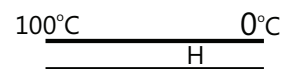
(b) In parallel thermal current distributes in the inverse ratio of resistance.

$$\text{Hence, } \frac{H_{\text{Cu}}}{H_{\text{Al}}} = \frac{R_{\text{Al}}}{R_{\text{Cu}}} = \frac{R_1}{R_2} = \frac{0.14}{0.08} = 1.75$$

**Example 4:** One end of a copper rod of length 1 m and area of cross section  $4.0 \times 10^{-4} \text{ m}^2$  is maintained at  $100^\circ\text{C}$ . At the end of rod ice is kept at  $0^\circ\text{C}$ . Neglecting the loss of heat from the surroundings, find the mass of ice melted in 1 h. Given  $k_{\text{cu}} = 401 \text{ W/m-K}$  and  $L_f = 3.35 \times 10^5 \text{ J/kg}$ .

**Sol:** Find total heat transfer in 1 hr time through rod and hence, melted ice can be found.

Thermal resistance of the rod,



$$R = \frac{1}{kA} = \frac{1.0}{(401)(4 \times 10^{-4})} = 6.23 \text{ K/W}$$

Heat Current  $H = \frac{\text{Temperature difference}}{\text{Thermal resistance}}$

$$= \frac{(100 - 0)}{6.23} = 16W$$

Heat transferred in 1 h,

$$Q = Ht = (16)(3600) = 57600 \text{ J} \quad \left( H = \frac{Q}{t} \right)$$

Now, let  $m$  mass of ice melts in 1 h, then

$$m = \frac{Q}{L} \quad (Q = mL)$$

$$= \frac{57600}{3.35 \times 10^5} = 0.172 \text{ kg} \quad \text{or} \quad 172 \text{ g}$$

**Example 5:** A body cools in 10 minutes from  $60^\circ\text{C}$  to  $40^\circ\text{C}$ . What will be its temperature after next 10 minutes? The temperature of the surrounding is  $10^\circ\text{C}$

**Sol:** Think of Newton's law of cooling.

According to Newton's law of cooling

$$\left( \frac{\theta_1 - \theta_2}{t} \right) = \alpha \left[ \left( \frac{\theta_1 + \theta_2}{2} \right) - \theta_0 \right]$$

For the given conditions,

$$\frac{60 - 40}{10} = \alpha \left[ \frac{60 + 40}{2} - 10 \right] \quad \dots (i)$$

Let be the temperature after next 10 minutes.

$$\text{Then } \frac{40 - \theta}{10} = \alpha \left[ \frac{40 + \theta}{2} - 10 \right] \quad \dots (ii)$$

Solving Eqs. (i) and (ii), we get  $\theta = 28^\circ\text{C}$

**Example 6:** Two bodies A and B have thermal emissivity of 0.01 and 0.81 respectively. The outer surface areas of the two bodies are same. The two bodies emit total radiant power at the same rate. The wavelength corresponding to maximum spectral radiancy from B is shifted from the wavelength corresponding to maximum spectral radiancy in the radiation from A by  $1.0 \mu\text{m}$ . If the temperature of A is  $5802 \text{ K}$ . calculate (a) The temperature of B,

(b) Wavelength  $\lambda_B$

**Sol:** Compare the emissive power of both and then temperature and  $\lambda_m$  of B can be calculated, Use  $\lambda_B - \lambda_A = 1 \mu\text{m}$ .

$$(a) P_A = P_B \quad \therefore e_A \sigma A_A T_A^4 = e_B \sigma A_B T_B^4$$

$$\therefore T_B = \left( \frac{e_A}{e_B} \right)^{\frac{1}{4}} T_A \quad \dots (A_A = A_B)$$

Substituting the values

$$T_B = \left( \frac{0.01}{0.81} \right)^{\frac{1}{4}} (5802) = 1934 \text{ K}$$

(b) According to Wein's displacement law,

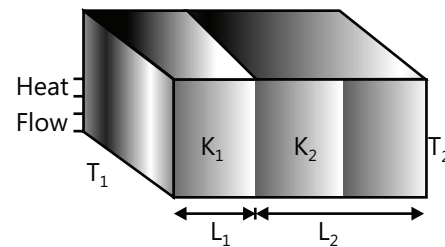
$$\lambda_A T_A = \lambda_B T_B$$

$$\therefore \lambda_B = \left( \frac{5802}{1934} \right) \lambda_A \quad \text{or} \quad \lambda_B = 3\lambda_A$$

$$\text{Also, } \lambda_B - \lambda_A = 1 \mu\text{m} \quad \text{or} \quad \lambda_B - \left( \frac{1}{3} \right) \lambda_B = 1 \mu\text{m}$$

$$\text{Or } \lambda_B = 1.5 \mu\text{m}$$

**Example 7:** Two plates each of area  $A$ , thickness  $L_1$  and  $L_2$  thermal conductivities  $K_1$  and  $K_2$  respectively are joined to form a single plate of thickness  $L_1 + L_2$ . If the temperatures of the free surfaces are  $T_1$  and  $T_2$ , calculate



(a) Rate of flow of heat

(b) Temperature of interface

(c) Equivalent thermal conductivity

**Sol:** Consider as thermal current where thermal resistors in series.

(a) If the thermal resistances of the two plates are  $R_1$  and  $R_2$  respectively then as plates are in series.

$$R_S = R_1 + R_2 = \frac{L_1}{AK_1} + \frac{L_2}{AK_2}$$

$$\text{As } R = \frac{L}{AK} \quad \text{and so}$$

$$H = \frac{dQ}{dt} = \frac{\Delta Q}{R} = \frac{(T_1 - T_2)}{(R_1 + R_2)} = \frac{A(T_1 - T_2)}{\left[ \frac{L_1}{K_1} + \frac{L_2}{K_2} \right]}$$

(b) If  $T$  is the common temperature of interface then as in series, rate of flow of heat remains same. i.e.  $H = H_1 (= H_2)$

$$\frac{T_1 - T_2}{R_1 + R_2} = \frac{T_1 - T}{R_1} \quad \text{i.e. } T = \frac{T_1 R_2 + T_2 R_1}{(R_1 + R_2)}$$

$$\text{or } T = \frac{\left[ T_2 \frac{L_1}{K_1} + T_1 \frac{L_2}{K_2} \right]}{\left[ \frac{L_1}{K_1} + \frac{L_2}{K_2} \right]}$$

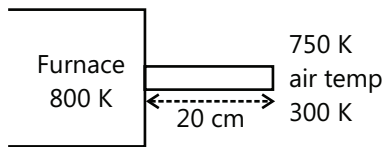
(c) If  $K$  is the equivalent conductivity of composite slab i.e. slab of thickness  $L_1 + L_2$  and cross sectional area  $A$ , then as in series

$$R_s = R_1 + R_2 \text{ or } \frac{(L_1 + L_2)}{AK_{eq}} = R_1 + R_2$$

$$K_{eq} = \frac{(L_1 + L_2)}{A(R_1 + R_2)} = \frac{L_1 + L_2}{\left[ \frac{L_1}{K_1} + \frac{L_2}{K_2} \right]} \text{ As } R = \frac{L}{AK}$$

**Example 8:** One end of a rod of length 20cm is inserted in a furnace at 800K. The sides of the rod are covered with an insulating material and the other end emits radiation like a black body. The temperature of this end is 750K in the steady state. The temperature of the surrounding air is 300K. Assuming radiation is the only important mode of energy transfer between the surrounding and the open end of the rod. Find the thermal conductivity of the rod. Stefan constant

$$\sigma = 6.0 \times 10^{-8} \text{ W/m}^2 \text{K}^4$$



**Sol:** Rate of heat through radiation would be equal to rate of heat transfer through rod.

Quantity of heat flowing through the rod per second in steady state

$$\frac{dQ}{dt} = \frac{K.A.d\theta}{x} \quad \dots (i)$$

Quantity of heat radiated from the end of the rod per second in steady state

$$\frac{dQ}{dt} = A\sigma(T^4 - T_0^4) \quad \dots (ii)$$

From Eqs. (i) and (ii),

$$\frac{K.d\theta}{x} = \sigma(T^4 - T_0^4)$$

$$\frac{K \times 50}{0.2} = 6.0 \times 10^{-8} [(7.5)^4 - (3)^4] \times 10^8$$

$$K = 74 \text{ W/mK}$$

**Example 9:** The lower surface of a slab of stone of face-area 3600 cm and thickness 10 cm is exposed to steam at 100°C. A block of ice at 0°C rests on the upper surface of slab. 4.8 g of ice melts in one hour. Calculate the thermal conductivity of the stone. Latent heat of fusion of ice =  $3.36 \times 10^5 \text{ Jkg}^{-1}$ .

**Sol:** Amount of heat transfer per second would be used to melt the mass of ice per second.

The amount of heat transferred through the slab to the ice in one hour is

$$Q = (4.8 \times 10^{-3} \text{ kg}) \times (3.36 \times 10^5 \text{ Jkg}^{-1}) \\ = 4.8 \times 336 \text{ J}$$

Using the equation  $Q = \frac{KA(\theta_1 - \theta_2)t}{x}$

$$4.8 \times 336 \text{ J} = \frac{K(3600 \text{ cm})^2 (100^\circ\text{C})(3600 \text{ s})}{10 \text{ cm}}$$

$$\text{or } K = 1.24 \times 10^{-3} \text{ Wm}^{-1}\text{C}^{-1}$$

**Example 10:** An icebox made of 1.5 cm thick Styrofoam has dimensions 60cm × 60cm × 30cm. It contains ice at 0°C and kept in a room at 40°C. Find the rate at which ice is melting. Latent heat of fusion of ice =  $3.36 \times 10^5 \text{ Jkg}^{-1}$  and thermal conductivity of Styrofoam =  $0.04 \text{ Wm}^{-1}\text{C}^{-1}$ .

**Sol:** Heat transfer through Styrofoam will melt the ice.

The total surface area of the walls

$$= 2(60 \text{ cm} \times 60 \text{ cm} + 60 \text{ cm} \times 30 \text{ cm} + 60 \text{ cm} \times 30 \text{ cm})$$

$$= 1.44 \text{ m}^2$$

The rate of heat flow into the box is

$$\frac{\Delta Q}{\Delta t} = \frac{KA(\theta_1 - \theta_2)}{x} \\ = \frac{(0.04 \text{ Wm}^{-1}\text{C}^{-1})(1.44 \text{ m}^2)(40^\circ\text{C})}{0.015 \text{ m}} = 154 \text{ W}$$

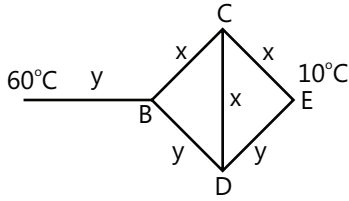
The rate at which the ice melts is

$$= \frac{154 \text{ W}}{3.36 \times 10^5 \text{ Jkg}^{-1}} = 0.46 \text{ gs}^{-1}$$

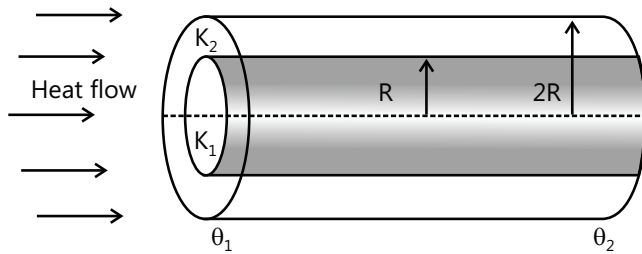
## JEE Advanced/Boards

**Example 1:** Three rods of the material  $x$  and three rods of material  $y$  are connected as shown in figure. All the rods are of identical length and cross sectional area. If the end A is maintained at 60°C and the junction E is

at 10°C Calculate temperature of junction B, C, D. the thermal conductivity of x is 0.92 cal/cm-s°C and that of y is 0.46 cal/cm-s°C.



**Sol:** Think of temperature drop across BCE and across BDE, temperature of C and D would be same as similar drop across BC and CE,



also across BD and DE. Thermal resistance  $R = \frac{1}{kA}$

$$\therefore \frac{R_x}{R_y} = \frac{k_y}{k_x} \quad (\text{as } l_x = l_y \text{ and } A_x = A_y)$$

$$\therefore \frac{R_x}{R_y} = \frac{0.46}{0.92} = \frac{1}{2}$$

So, if  $R_x = R$  then  $R_y = 2R$

CEDB forms a balanced Wheatstone bridge i.e.

$T_C = T_D$  and no heat flows through CD

$$\therefore \frac{1}{R_{BE}} = \frac{1}{R+R} + \frac{1}{2R+2R} \text{ or } R_{BE} = \frac{4}{3}R$$

The total resistance between A and E will be,

$$R_{AE} = R_{AB} + R_{BE} = 2R + \frac{4}{3}R = \frac{10}{3}R$$

$\therefore$  Heat current between A and E is

$$H = \frac{(\Delta T)}{R_{AE}} = \frac{(60-10)}{(\frac{10}{3})R} = \frac{15}{R}$$

Now, if  $T_B$  is the temperature at B,

$$H_{AB} = \frac{(\Delta T)_{AB}}{R_{AB}} \text{ or } \frac{15}{R} = \frac{60-T_B}{2R} \text{ or } T_B = 30^\circ\text{C}$$

$$\text{Further, } H_{AB} = H_{BC} + H_{BD} \text{ or } \frac{15}{R} = \frac{30-T_C}{R} + \frac{30-T_D}{2R}$$

(Say  $T_C = T_D = T$ )

$$\text{Or } 15 = (30-T) + \frac{(30-T)}{2}$$

Solving this we get  $T = 20^\circ\text{C}$  or  $T_C = T_D = 20^\circ\text{C}$

**Example 2:** A cylinder of radius R made of a thermal conductivity  $K_1$  is surrounded by cylindrical shell of inner radius R and another radius 2R made of a material of thermal conductivity  $K_2$ . The two ends of the combined system are maintained at two different temperatures. There is no loss of heat across the cylindrical surface and system is in steady state. What is the effective thermal conductivity of system?

**Sol:** Assume this to parallel combination of thermal resistors. As both have same temperature across their ends.

In this situation a rod of length L and area of cross section  $\pi R^2$  and another of same length L and area of cross-section  $\pi[(2R)^2 - R^2] = 3\pi R^2$  will conduct heat simultaneously so total heat flowing per second will be,

$$\begin{aligned} \frac{dQ}{dt} &= \frac{dQ_1}{dt} + \frac{dQ_2}{dt} \\ &= \frac{K_1 \pi R^2 (\theta_1 - \theta_2)}{L} + \frac{K_2 3\pi R^2 (\theta_1 - \theta_2)}{L} \end{aligned} \quad \dots(i)$$

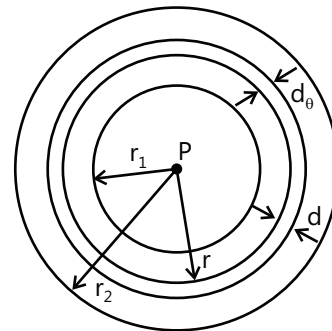
Now, if the equivalent conductivity is K then,

$$\frac{dQ}{dt} = K \frac{4\pi R^2 (\theta_1 - \theta_2)}{L} \quad [\text{As } A = \pi(2R)^2] \quad \dots(ii)$$

So, from Eqs. (i) and (ii), we have

$$4K = K_1 + 3K_2 \quad \text{i.e. } K = \frac{(K_1 + 3K_2)}{4}$$

**Example 3:** A point source of heat of power P is placed at the center of a spherical shell of mean radius R. the material of the shell has thermal conductivity k. calculate the thickness of the shell if temperature difference between the outer and inner surfaces of the shell in steady state is T.



**Sol:** Total thermal resistance  $\int \frac{dr}{k4\pi r^2} = \left( \frac{l}{KA} \right)$ . Power

of source equal to rate of heat transfer at steady state.

Consider a concentric spherical shell of radius  $r$  and thickness  $dr$  as shown in figure. In steady state, the rate of heat flow (heat current) through this shell will be,

$$H = \frac{\Delta T}{R} = \frac{(-d\theta)}{\frac{dr}{(k)(4\pi r^2)}} \left( R = \frac{1}{kA} \right)$$

$$\text{or } H = -(4\pi kr^2) \frac{d\theta}{dr}$$

Here, negative sign is used because with increase in  $r$ , decreases.

$$\therefore \int_{r_1}^{r_2} \frac{dr}{r^2} = -\frac{4\pi k}{H} \int_{\theta_1}^{\theta_2} d\theta$$

$$\text{This equation gives, } H = \frac{4\pi kr_1 r_2 (\theta_1 - \theta_2)}{(r_2 - r_1)}$$

$$\text{In steady state, } H = P, r_1 r_2 = R^2 \quad \text{and} \quad \theta_1 - \theta_2 = T$$

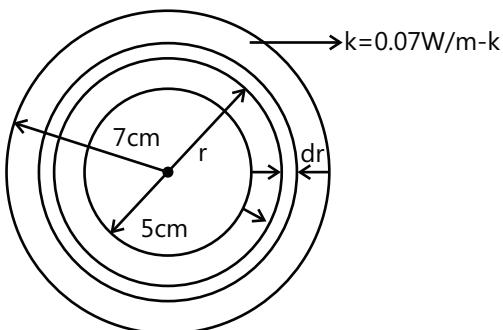
$$\therefore \text{Thickness of shell, } r_2 - r_1 = \frac{4\pi k R^2 T}{P}$$

**Example 4:** A steam pipe of radius 5cm carries steam at 100°C. The pipe is covered by a jacket of insulating material 2cm thick having a thermal conductivity 0.07 W/m-K. If the temperature at the outer wall of the pipe jacket is 20°C, how much heat is lost through the jacket per meter length in an hour?

**Sol:** Heat lost through curved surface of the pipe.

$$R_{\text{thermal}} = \int \frac{dr}{K2\pi r l} \text{ for pipe of length } l.$$

Thermal resistance per meter length of an element at distance  $r$  of thickness  $dr$  is



$$dR = \frac{dr}{k(2\pi r)} \quad \left( R = \frac{1}{kA} \right)$$

$$\therefore \text{Total resistance } R = \int_{r_1=5\text{cm}}^{r_2=7\text{cm}} dR$$

$$= \frac{1}{2\pi k} \int_{5 \times 10^{-2} \text{m}}^{7 \times 10^{-2} \text{m}} \frac{dr}{r} = \frac{1}{2\pi k} \ln \left( \frac{7}{5} \right)$$

$$= \frac{1}{2\pi(0.07)} \ln(1.4) = 0.765 \text{ K/W}$$

$$\text{Heat current } H = \frac{\text{Temperature difference}}{\text{Thermal resistance}}$$

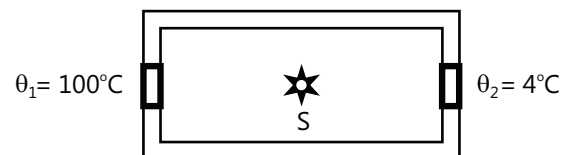
$$= \frac{(100 - 20)}{0.765} = 104.6 \text{ W}$$

$\therefore$  Heat lost in one hour = Heat current  $\times$  time

$$= (104.6)(3600) \text{ J} = 3.76 \times 10^5 \text{ J}$$

**Example 5:** A closed cubical box is made of perfectly insulating material and the only way for heat to enter or leave the box is through two solid cylindrical metal plugs, each of cross sectional area 12 cm<sup>2</sup> and length 8 cm fixed in the opposite walls of the box. The outer surface of the plug is kept at a temperature of 100°C while the outer surface of the other plug is maintained at a temperature of 4°C. The thermal conductivity of the material of the plug is 2.0 Wm<sup>-1</sup> °C<sup>-1</sup>. A source of energy generating 13 W is enclosed inside the box. Find the equilibrium temperature of the inner surface of the box assuming that it is the same at all points on the inner surface.

**Sol:** At steady state, rate of heat transfer through both plugs would be same.



The situation is shown in figure. Let the temperature inside the box be  $\theta$ . The rate at which heat enters the

$$\text{box through the left plug is } \frac{\Delta Q_1}{\Delta t} = \frac{KA(\theta_1 - \theta)}{x}$$

The rate of heat generation in the box = 13 W. The rate at which heat flows out of the box through the right plug is

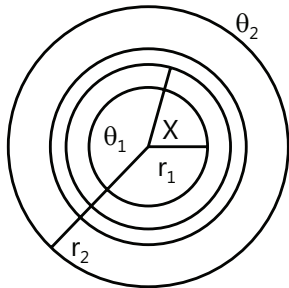
$$\frac{\Delta Q_2}{\Delta t} = \frac{KA(\theta - \theta_2)}{x}$$

$$\text{In the steady state } \frac{\Delta Q_1}{\Delta t} + 13 \text{ W} = \frac{\Delta Q_2}{\Delta t}$$

$$\text{or, } \frac{KA}{x}(\theta_1 - \theta) + 13 \text{ W} = \frac{KA}{x}(\theta - \theta_2)$$

$$\begin{aligned} \text{or, } 2 \frac{KA}{x} \theta &= \frac{KA}{x} (\theta_1 + \theta_2) + 13W \\ \text{or, } \theta &= \frac{\theta_1 + \theta_2}{2} + \frac{(13W)x}{2KA} \\ &= \frac{100^\circ\text{C} + 4^\circ\text{C}}{2} + \frac{(13W) \times 0.08\text{m}}{2 \times (2.0\text{Wm}^{-1}\text{C}^{-1})(12 \times 10^{-4}\text{m}^2)} \\ &= 52^\circ\text{C} + 216.67^\circ\text{C} = 269^\circ\text{C} \end{aligned}$$

**Example 6:** Two thin metallic spherical shells of radii  $r_1$  and  $r_2$  ( $r_1 < r_2$ ) are placed with their centres coinciding. A material of thermal conductivity  $K$  is filled in the space between the shells. The inner shell is maintained at temperature and the outer shell at temperature  $\theta_1$  ( $\theta_1 < \theta_2$ ). Calculate the rate at which heat flows radially through the material.



**Sol:** Heat flowing radially outward through spherical shells. Both connected in series.

Let us draw two spherical shells of radii  $x$  and  $x+dx$  concentric with the given system. Let the temperatures at these shells be  $\theta$  and  $\theta + d\theta$  respectively. The amount of heat flowing radially inward through the material between  $x$  and  $x+dx$  is

$$\frac{\Delta Q}{\Delta t} = \frac{K4\pi x^2}{dx} \cdot dQ$$

Thus,

$$K4\pi \int_{\theta_1}^{\theta_2} d\theta = \frac{\Delta Q}{\Delta t} \int_{r_1}^{r_2} \frac{dx}{x^2}$$

$$\text{or, } K4\pi(\theta_2 - \theta_1) = \frac{\Delta Q}{\Delta t} \left( \frac{1}{r_1} - \frac{1}{r_2} \right)$$

$$\text{or, } \frac{\Delta Q}{\Delta t} = \frac{K4\pi r_1 r_2 (\theta_2 - \theta_1)}{r_2 - r_1}$$

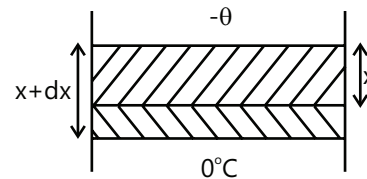
**Example 7:** The temperature of air above a lake is  $-10^\circ\text{C}$ . At some instant, the thickness of ice in the lake is

2 cm. calculate the time required for the thickness to be doubled. Thermal conductivity ice =  $0.004\text{cal/cm/s}^\circ\text{C}$ , density of ice =  $0.92\text{g/cm}^3$  and latent heat of ice =  $80\text{cal/g}$ .

**Sol:** Amount of Heat transfer through ice at any time would result in freezing the water of lake. Proceed with assuming Area of lake =  $A$ , eventually it will cancel out.

As the temperature of air is below  $0^\circ\text{C}$ , water begins to freeze to form a layer of ice. The thickness of the layer gradually increases.

Consider that a layer of thickness  $x$  has already been formed on a lake at  $0^\circ\text{C}$ . Let  $A$  be the area of the layer,  $L$  the latent heat of ice and  $\rho$  its density. The amount of heat required when the thickness of ice increases by  $dx$  is



$$Q = mL = (Adx\rho)L$$

This quantity of heat is conducted upwards through the layer in time  $dt$  when the temperature of air is  $-\theta$ .

$$\therefore A\rho Ldx = \frac{KA(0 - (-\theta))}{x} dt; \frac{dx}{dt} = \frac{K\theta}{\rho Lx}; dt = \frac{\rho Lx dx}{K\theta}$$

Time taken  $t$  for the thickness to increase from  $x_1$  and  $x_2$  to is obtained by integrating

$$t = \int_0^t dt = \frac{\rho L}{K\theta} \int_{x_1}^{x_2} x dx \quad \text{Or}$$

$$t = \frac{\rho L}{2K\theta} (x_2^2 - x_1^2) \quad \therefore t = \frac{0.92 \times 80}{2 \times 0.004 \times 10} (4^2 - 2^2)$$

$$= 11040\text{s} = 3.07\text{hr}$$

**Example 8:** A liquid placed in a container open to atmosphere takes 5 minutes to cool from  $80^\circ\text{C}$  to  $50^\circ\text{C}$ . How much time will it take to cool from  $60^\circ\text{C}$  to  $30^\circ\text{C}$ ? The temperature of the surroundings is  $20^\circ\text{C}$ .

**Sol:** Newton's law of cooling.

The rate of cooling of a body at temperature  $T$  is given

$$\text{by Newton's law of cooling as } \frac{dT}{dt} = -K(T - T_0)$$

Where  $K$  is a constant for the body and  $T_0$  is the temperature of the surroundings.

$$\frac{T - T_0}{dT} = -Kdt$$

The negative sign indicates that the temperature is falling.

$$\text{Integrating, we get } \int_{T_1}^{T_2} \frac{dT}{T - T_0} = -K \int_0^t dt$$

$$\log_e \left( \frac{T_2 - T_0}{T_1 - T_0} \right) = -Kt$$

As  $t = 5, T_1 = 80^\circ\text{C}, T_2 = 50^\circ\text{C}, T_0 = 20^\circ\text{C}$

$$\therefore 5 = \frac{1}{K} \log_e \left( \frac{80 - 20}{50 - 20} \right)$$

$$\text{or } 5K = \log_e(2) \quad \dots (i)$$

If  $t$  is time taken when

$$T_1 = 60^\circ\text{C} \text{ and } T_2 = 30^\circ\text{C}$$

$$Kt = \log_e \left( \frac{60 - 20}{30 - 20} \right) \quad \dots (ii)$$

$$\text{or } Kt = \log_e(4)$$

Dividing equation (ii) by equation (i)

$$\frac{t}{5} = \frac{\log_e 4}{\log_e 2} = \frac{1.386}{0.693} = 2 \quad \text{or } t = 10 \text{ minutes}$$

**Example 9:** A solid copper sphere cools at the rate of  $2.8^\circ\text{C}$  per minute, when its temperature is  $127^\circ\text{C}$ . Find the rate at which another copper sphere of twice the radius will lose its temperature at  $327^\circ\text{C}$ , if in both the cases, the room temperature is maintained at  $27^\circ\text{C}$ .

**Sol:** Get the rate of heat loss through radiations.

$$\text{The rate of loss of heat} = \frac{dQ}{dt} = ms \frac{dT}{dt}$$

$$= \sigma A(T^4 - T_0^4) \text{ or } \frac{dT}{dt} = \frac{\sigma A}{ms}(T^4 - T_0^4)$$

If  $r$  is radius of sphere is  $r$ , then  $m = \frac{4}{3}\pi r^3 \times \rho$

Where  $\rho$  is density and  $s$  is specific heat

$$\frac{dT}{dt} = \frac{\sigma \times 4\pi r^2}{\frac{4}{3}\pi r^3 \rho \times s}(T^4 - T_0^4) = \frac{3\sigma}{r\rho \times s}(T^4 - T_0^4)$$

$$\left( \frac{dT}{dt} \right)_{127^\circ\text{C}} = 2.8 = \frac{3\sigma}{r\rho \times s}(400^4 - 300^4) \quad \dots (i)$$

For the second sphere of radius  $2r$

$$\left( \frac{dT}{dt} \right)_{327^\circ\text{C}} = \frac{3\sigma}{(2r)\rho \times s}(600^4 - 300^4) \quad \dots (ii)$$

Dividing equation (ii) by equation (i), we get

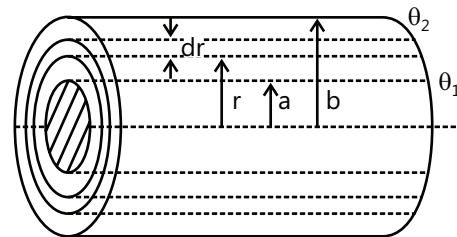
$$\left( \frac{dT}{dt} \right)_{327^\circ\text{C}} = \frac{2.8}{2} \left[ \frac{6^4 - 3^4}{4^4 - 3^4} \right] = 9.72^\circ\text{C / minute}$$

**Example 10:** A 2m long wire of resistance 4 ohm and diameter 0.64 mm is coated with plastic insulation of thickness 0.06 mm. When a current of 5 ampere flows through the wire, find the temperature difference across insulation in steady state if

$$[K = 0.16 \times 10^{-2} \text{ cal / cm} - ^\circ\text{Cs}]$$

**Sol:** Tricky one! Rate of heat generation in the wire due to flow of current must be same as rate of heat transfer through plastic insulation.

Considering a concentric cylindrical shell of radius  $r$  and thickness  $dr$  as shown in figure. The radial rate of flow of heat through this shell in steady state will be



$$H = \frac{dQ}{dt} = -KA \frac{d\theta}{dr}$$

Negative sign is used as with increase in  $r$ ,  $\theta$  decreases

Now as for cylindrical shell  $A = 2\pi rL$

$$H = -2\pi rLK \frac{d\theta}{dr}$$

$$\text{or } \int_a^b \frac{dr}{r} = -\frac{2\pi rLK}{H} \int_{\theta_1}^{\theta_2} d\theta$$

Which on integration and simplification gives

$$H = \frac{dQ}{dt} = -\frac{2\pi LK(\theta_1 - \theta_2)}{\ln(b/a)} \quad \dots (i)$$

$$\text{Here, } H = \frac{I^2 R}{4.2} = \frac{(5)^2 \times 4}{4.2} = 24 \frac{\text{cal}}{\text{s}}$$

$$L = 2\text{m} = 200\text{cm}$$

$$r_1 = (0.64/2) = 0.032\text{cm}$$

$$\text{and } R_2 = r_1 + d = 0.032 + 0.006 = 0.038$$

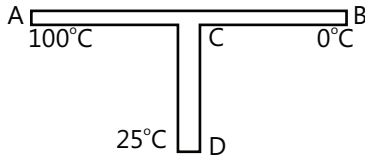
$$\text{So } (\theta_1 - \theta_2) = \frac{24 \times \ln\left(\frac{38}{32}\right)}{2 \times 2.3026 [\log_{10} 38 - \log_{10} 32]}$$



$$= \frac{24 \times 2.3026 [\log_{10} 38 - \log_{10} 32]}{3.14 \times 0.64}$$

$$\text{or } (\theta_1 - \theta_2) = \frac{55 \times [1.57 - 1.50]}{2} = 2^\circ\text{C}.$$

**Example 11:** A rod CD of thermal resistance  $5.0\text{KW}^{-1}$  is joined at the middle of an identical rod AB as shown in figure. The ends A, B and D are maintained at  $100^\circ\text{C}$ ,  $0^\circ\text{C}$ , and  $25^\circ\text{C}$  respectively. Find the heat current in CD.



**Sol:** At point C, total thermal current inflow equal to total thermal current out flow.

The thermal resistance of AC is equal to that of CB and is equal to  $2.5\text{KW}^{-1}$ . Suppose, the temperature at C is  $\theta$ . The heat current through AC, CB, and CD are

$$\frac{\Delta Q_1}{\Delta t} = \frac{100^\circ\text{C} - \theta}{2.5\text{KW}^{-1}};$$

$$\frac{\Delta Q_2}{\Delta t} = \frac{\theta - 0^\circ\text{C}}{2.5\text{KW}^{-1}} \text{ and } \frac{\Delta Q_3}{\Delta t} = \frac{\theta - 25^\circ\text{C}}{5.0\text{KW}^{-1}}$$

We also have

$$\frac{\Delta Q_1}{\Delta t} = \frac{\Delta Q_2}{\Delta t} + \frac{\Delta Q_3}{\Delta t}$$

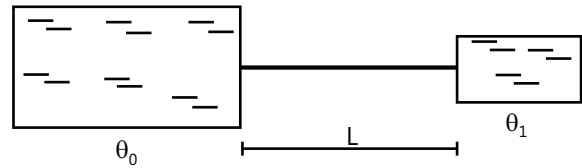
$$\text{or, } \frac{100^\circ\text{C} - \theta}{2.5} = \frac{\theta - 0^\circ\text{C}}{2.5} + \frac{\theta - 25^\circ\text{C}}{5.0}$$

$$\text{or, } 225^\circ\text{C} = 5\theta$$

$$\text{or, } \theta = 45^\circ\text{C}$$

$$\text{Thus, } \frac{\Delta Q_3}{\Delta t} = \frac{45^\circ\text{C} - 25^\circ\text{C}}{5.0\text{KW}^{-1}} = \frac{20\text{K}}{5.0\text{KW}^{-1}} = 4.0\text{W}.$$

**Example 12:** Figure shows a large tank of water at a constant temperature  $\theta_0$  and a small vessel containing a mass  $m$  of water at an initial temperature  $\theta_1$  ( $<\theta_0$ ). A metal rod of length  $L$ , area cross section  $A$  and thermal conductivity  $K$  connects the two vessels. Find the time taken for the temperature of the water in the smaller vessel become  $\theta_2$  ( $\theta_1 < \theta_2 < \theta_0$ ). Specific heat capacity of water is  $s$  and all other heat capacities are negligible.



**Sol:** Rate of heat transfer is variable as temperature of small vessel will be changing.

Suppose, the temperature of the water in the smaller vessel is at time  $t$ . In the next time interval  $dt$ , a heat  $dQ$  is transferred to it where

$$\Delta Q = \frac{KA}{L}(\theta_0 - \theta) dt. \quad \dots (i)$$

This heat increases the temperature of the water of mass  $m$  to  $\theta + d\theta$  where

$$\Delta Q = ms d\theta \quad \dots (ii)$$

From (i) and (ii),

$$\frac{KA}{L}(\theta_0 - \theta) dt = ms d\theta$$

$$\text{or, } dt = \frac{Lms}{KA} \frac{d\theta}{\theta_0 - \theta} \quad \text{or, } \int_0^T dt = \frac{Lms}{KA} \int_{\theta_1}^{\theta_2} \frac{d\theta}{\theta_0 - \theta}$$

Where  $T$  is the time required for the temperature of the water to become.

$$\text{Thus, } T = \frac{Lms}{KA} \ln \frac{\theta_0 - \theta_1}{\theta_0 - \theta_2}$$

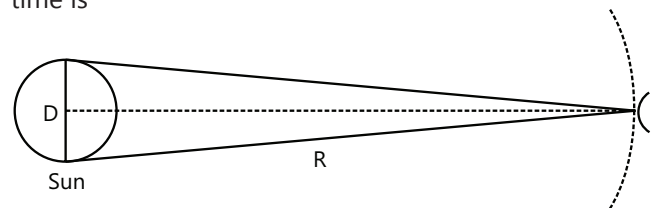
**Example 13:** The earth receives solar radiation at a rate of  $8.2 \text{ J cm}^{-2} \text{ min}^{-1}$ . Assuming that the sun radiates like a blackbody, calculate surface temperature of the sun. The angle subtended by the sun on the earth is  $0.53^\circ$  and Stefan constant  $\sigma = 5.67 \times 10^{-8} \text{ Wm}^{-2}\text{K}^{-4}$ .

**Sol:** Think of intensity of thermal heat out a distance  $R$  from the source.

Let the diameter of the sun be  $D$  and its distance from the earth be  $R$ . From the question,

$$\frac{D}{R} = 0.53 \times \frac{\pi}{180} = 9.25 \times 10^{-3} \dots (i)$$

The radiation emitted by the surface of the sun per unit time is



$$4\pi \left(\frac{D}{2}\right)^2 \sigma T^4 = \pi D^2 \sigma T^4$$

At distance  $R$ , this radiation falls on an area of  $4\pi R^2$  in unit time. The radiation received at the earth's surface per unit time per unit area is, therefore,

$$\frac{\pi D^2 \sigma T^4}{4\pi R^2} = \frac{\sigma T^4}{4} \left(\frac{D}{R}\right)^2$$

$$\text{Thus, } \frac{\sigma T^4}{4} \left(\frac{D}{R}\right)^2 = 8.2 \text{ Jcm}^{-2} \text{ min}^{-1}$$

$$\text{or, } \frac{1}{4} \times (5.67 \times 10^{-8} \text{ Wm}^{-2}\text{K}^{-4}) T^4 \times$$

$$(9.25 \times 10^{-3})^2 \times T^4$$

$$= \frac{8.2}{10^{-4} \times 60} \text{ Wm}^{-2}$$

$$\text{or, } T = 5794\text{K} \approx 5800\text{K}$$

**Example 14:** On a cold winter day, the atmospheric temperature is  $\theta$  (on Celsius scale) which is below  $0^\circ\text{C}$ . A cylindrical drum of height  $h$  made of a bad conductor is completely filled with water at  $0^\circ\text{C}$  and is kept outside without any lid. Calculate the time taken for the whole mass of water to freeze. Thermal conductivity of ice is  $K$  and its latent heat of fusion is  $L$ . Neglect expansion of water on freezing.

**Sol:** Rate of heat transfer would be dependent on thickness of layer of ice. Write equation of heat transfer at any time 't' when thickness of ice is 'x'.

Suppose, the ice starts forming at time  $t=0$  and a thickness  $x$  is formed at time  $t$ . The amount of heat flown from the water to the surrounding in the time interval  $t$  to  $t+dt$  is

$$\Delta Q = \frac{KA\theta}{x} dt.$$

The mass of the ice formed due to the loss of this amount of heat is

$$dm = \frac{\Delta Q}{L} = \frac{KA\theta}{xL} dt.$$

The thickness  $dx$  of ice formed in time  $dt$  is

$$dx = \frac{dm}{A\rho} = \frac{KA\theta}{\rho xL} dt \quad \text{or,} \quad dt = \frac{\rho L}{K\theta} x dx.$$

Thus, the time  $T$  taken for the whole mass of water to freeze is given by

$$\int_0^T dt = \frac{\rho L}{K\theta} \int_0^h x dx \quad \text{or,} \quad T = \frac{\rho L h^2}{2K\theta}$$

**Example 15:** A thermometer is taken from a room that is  $20^\circ\text{C}$  to the outdoors where the temperature is  $5^\circ\text{C}$ . After one minute, the thermometer reads  $12^\circ\text{C}$ . Use Newton's law of cooling to answer following questions. (a) What will the reading on the thermometer be after one more minute?

(b) When will the thermometer read  $6^\circ\text{C}$ ?

**Sol:** Get the 'k' for Newton's law of cooling by given condition, then the all desired value.

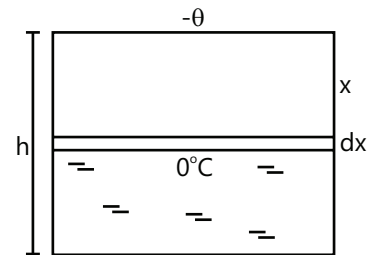
If  $T$  is the thermometer temperature, then Newton's law of cooling tells us that

$$\frac{dT}{dt} = k(5 - T); \quad T(0) = 20.$$

The solution of this initial value problem is

$$T = 5 + 15e^{-kt}.$$

We still need to find the value of  $k$ . We can do this by using the given information that  $T(1)=12$ . In fact, let us pause here to consider the general problem of finding the value of  $k$ . We will obtain some facts that can be used in the rest of the problems involving Newton's law of cooling.



Suppose that we have the model

$$\frac{dT}{dt} = k(T_s - T); \quad T(0) = T_0 \\ T(t_1) = T_1$$

Where  $t_1$  is some time other than 0. then the first two equations in the model, we obtain  $T = T_s + (T_0 - T_s)e^{-kt}$  and from the third equation we obtain

$$T_s + (T_0 - T_s)e^{-kt_1} = T_1$$

$$\text{Thus, } (T_0 - T_s)e^{-kt_1} = T_1 - T_s$$

which gives us

$$e^{-kt_1} = \frac{T_1 - T_s}{T_0 - T_s} \quad \text{or} \quad e^{kt_1} = \frac{T_0 - T_s}{T_1 - T_s}$$

$$\text{or } k = \frac{1}{t_1} \ln \left( \frac{T_0 - T_s}{T_1 - T_s} \right)$$

The latter equations give us the value of  $k$ . However, note that, in most problems that we deal with, it is not really necessary to find the value of  $k$ . Since the term

$e^{-kt}$  that appears in the solution of Newton's Law of cooling can be written as  $e^{-kt} = (e^{-kt_1})^{t/t_1}$

We really just need (in most situations) to know the value of  $e^{-kt_1}$ , and this value has been obtained in the work done above. In particular, the solution of Newton's Law of Cooling,

$$T = T_s + (T_0 - T_s)e^{-kt}$$

Can be written as

$$T = T_s + (T_0 - T_s)(e^{-kt_1})^{t/t_1}$$

or as  $T = T_s + (T_0 - T_s) \left( \frac{T_1 - T_s}{T_0 - T_s} \right)^{t/t_1}$

$$T = T_s + (T_0 - T_s) \left( \frac{T_1 - T_s}{T_0 - T_s} \right)^{t/t_1}$$

Returning now to the problem at hand (with the thermometer), we see that temperature function for

the thermometer is  $T = 5 + 15 \left( \frac{7}{15} \right)^t$ .

Note that this makes sense because this formula gives

us  $T(0) = 5 + 15 \left( \frac{7}{15} \right)^0 = 20$ .

And  $T(1) = 5 + 15 \left( \frac{7}{15} \right)^1 = 12$ .

To find what the thermometer will read two minutes after being taken outside, we compute

$$T(2) = 5 + 15 \left( \frac{7}{15} \right)^2 \approx 8.3.$$

This tells us that the thermometer will read about  $8.3^\circ\text{C}$  two minutes after being taken outside.

Finally, to determine when the thermometer will read  $6^\circ\text{C}$ , we solve the equation

$$5 + 15 \left( \frac{7}{15} \right)^t = 6$$

The step-by-step solution of this equation is

$$15 \left( \frac{7}{15} \right)^t = 1 \left( \frac{7}{15} \right)^t = \frac{1}{15}$$

$$\ln \left( \left( \frac{7}{15} \right)^t \right) = \ln \left( \frac{1}{15} \right); t \ln \left( \frac{7}{15} \right) = \ln \left( \frac{1}{15} \right)$$

$$t = \frac{\ln(1/15)}{\ln(7/15)} \approx 3.5.$$

Thus, the thermometer will reach  $6^\circ\text{C}$  after being outside for about 3.5 minutes.

## JEE Main/Boards

### Exercise 1

- Q.1** Which metal is the best conductor of heat?
- Q.2** Which mode of transfer of heat is quickest?
- Q.3** What is temperature gradient?
- Q.4** How can heat be transferred from one place to other?
- Q.5** What are the basic differences between conduction, convection and radiation?
- Q.6** What are the thermal radiations? From where do you obtain them? How do they transfer from one place to another?
- Q.7** Discuss the variation of temperature of the hot body with time during cooling process. What do you conclude from this?
- Q.8** What is meant by thermal conductivity and its coefficient? What are its SI units and CGS units?
- Q.9** Explain Newton's law of cooling and discuss its experimental verification.
- Q.10** Thickness of ice on a lake is 5 cm. and the temperature of air is  $-20^\circ\text{C}$ . If the rate of cooling of

water inside the lake be  $20000 \text{ cal min}^{-1}$  through each square meter surface, find  $K$  of ice?

**Q.11** A metal plate 4 mm thick has a temp difference of  $32^\circ\text{C}$  between its faces. It transmits  $200 \text{ kcal h}^{-1}$  through an area of  $5 \text{ cm}^2$ . Calculate thermal conductivity of the material of the plate.

**Q.12** Estimate the rate at which ice would melt in a wooden box 2.5 cm thick and of inside measurements  $100 \times 60 \times 40 \text{ cm}$ , assuming that the external temperature is  $32^\circ\text{C}$  and coefficient of thermal conductivity of wood is  $0.168 \text{ Wm}^{-1} \text{ K}^{-1}$ . Given  $L=80 \text{ cal/g}$ .

**Q.13** A pan filled with hot food cools from  $94^\circ\text{C}$  to  $86^\circ\text{C}$  in 2 minutes when the room temperature is at  $20^\circ\text{C}$ . How long will it take to cool from  $71^\circ\text{C}$  to  $69^\circ\text{C}$ ? Here cooling takes place according to Newton's law of cooling.

**Q.14** A liquid initially at  $70^\circ\text{C}$  cools to  $55^\circ\text{C}$  in 5 minutes and  $45^\circ\text{C}$  in 10 minutes. What is the temperature of the surroundings?

## Exercise 2

### Single Correct Choice Type

**Q.1** Four rods of same material with different radii  $r$  and length  $l$  are used to connect two reservoirs of heat at different temperatures. Which one will conduct most heat?

- (A)  $r=2 \text{ cm}, l=0.5 \text{ m}$     (B)  $r=2 \text{ cm}, l=2 \text{ m}$   
 (C)  $r=0.5 \text{ cm}, l=0.5 \text{ m}$     (D)  $r=1 \text{ cm}, l=1 \text{ m}$

**Q.2** A wall has two layers A and B each made of different materials, both the layers have same thickness. The thermal conductivity of the material A is twice of that of B. Under thermal equilibrium, the temperature difference across the wall B is  $36^\circ\text{C}$ . The temperature difference across wall A is

- (A)  $6^\circ\text{C}$     (B)  $12^\circ\text{C}$     (C)  $18^\circ\text{C}$     (D)  $72^\circ\text{C}$

**Q.3** A black metal foil is warmed by radiation from a small sphere at temperature 'T' and at a distance 'd'. It is found that the power received by the foil is P. If both

the temperature and distance are doubled, the power received by the foil will be

- (A)  $16 P$     (B)  $4 P$     (C)  $2 P$     (D)  $P$

**Q.4** The rate of emission of radiation of a black body at  $273^\circ\text{C}$  is E, then the rate of emission of radiation of this body at  $0^\circ\text{C}$  will be

- (A)  $\frac{E}{16}$     (B)  $\frac{E}{4}$     (C)  $\frac{E}{8}$     (D) 0

**Q.5** The power radiated by a black body is P and it radiates maximum energy around the wavelength  $\lambda_0$ . If the temperature of the black body is now changed so that it radiates maximum energy around wavelength  $3/4 \lambda_0$ , the power radiated by it will increase by a factor of

- (A)  $4/3$     (B)  $16/9$     (C)  $64/27$     (D)  $256/81$

**Q.6** Star S1 emits maximum radiation of wavelength 420 nm and the star S2 emits maximum radiation of wavelength 560 nm, what is the ratio of the temperature of S1 and S2

- (A)  $4/3$     (B)  $(4/3)^{1/4}$     (C)  $3/4$     (D)  $(3/4)^{1/2}$

**Q.7** Spheres P and Q are uniformly constructed from the same material which is a good conductor of heat and the radius of Q is thrice the radius of P. the rate of fall of temperature of P is x times that of Q when both are at the same surface temperature. The value of x is

- (A)  $1/4$     (B)  $1/3$     (C) 3    (D) 4

**Q.8** A black body calorimeter filled with hot water cools from  $60^\circ\text{C}$  to  $50^\circ\text{C}$  in 4 min and  $40^\circ\text{C}$  to  $30^\circ\text{C}$  in 8 min. The approximate temperature of surrounding is

- (A)  $10^\circ\text{C}$     (B)  $15^\circ\text{C}$     (C)  $20^\circ\text{C}$     (D)  $25^\circ\text{C}$

**Q.9** A system S receives heat continuously from an electrical heater of power 10W. The temperature of S becomes constant at  $50^\circ\text{C}$ . When the surrounding temperature is  $20^\circ\text{C}$ . After the heater is switched off, S cools from  $35.1^\circ\text{C}$  to  $34.9^\circ\text{C}$  in 1 minute. The heat capacity of S is

- (A)  $100 \text{ J}/^\circ\text{C}$     (B)  $300 \text{ J}/^\circ\text{C}$   
 (C)  $750 \text{ J}/^\circ\text{C}$     (D)  $1500 \text{ J}/^\circ\text{C}$

## Previous Years' Questions

**Q.1** A cylinder of radius  $R$  made of a material of thermal conductivity  $K_1$  is surrounded by a cylindrical shell of inner radius  $R$  and outer radius  $2R$  made of a material of thermal conductivity  $K_2$ . The two ends of the combined system are maintained at two different temperatures. There is loss of heat across the cylindrical surface and the system is in steady state. The effective thermal conductivity of the system is \_\_\_\_\_. (1988)

**Q.2** Two metallic spheres  $S_1$  and  $S_2$  are made of the same material and have got identical surface finish. The mass of  $S_1$  is thrice that of  $S_2$ . Both the spheres are heated to the same high temperature and placed in the same room having lower temperature but are thermally insulated from each other. The ratio of the initial rate of cooling of  $S_1$  to that  $S_2$  is \_\_\_\_\_. (1995)

**Q.3** The intensity of radiation emitted by the sun has its maximum value at a wavelength of  $510 \text{ nm}$  and that emitted by the North Star has the maximum value at  $350 \text{ nm}$ . If these stars behave like blackbodies, then the ratio of the surface temperature of the North Star is \_\_\_\_\_. (1997)

**Q.4** A spherical black body with radius of  $12 \text{ cm}$  radiates  $450 \text{ W}$  power at  $500 \text{ K}$ . If the radius were halved and the temperature doubled, the power radiated would be \_\_\_\_\_. (1997)

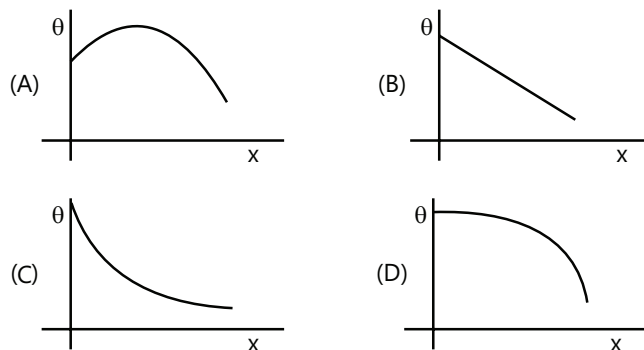
**Q.5** A black body is at temperature of  $2880 \text{ K}$ . The energy of radiation emitted by this body with wavelength between  $499 \text{ nm}$  and  $500 \text{ nm}$  is  $U_1$ , between  $999 \text{ nm}$  and  $1000 \text{ nm}$  is  $U_2$  and between  $1499 \text{ nm}$  and  $1500 \text{ nm}$  is  $U_3$ . The Wien constant,  $b = 2.88 \times 10^6 \text{ nm-K}$ . Then, what can be inferred about the relation between the energies? (1998)

**Q.6** Two identical conducting rods are first connected independently to two vessels, one containing water at  $100^\circ\text{C}$  and the other containing ice at  $0^\circ\text{C}$ . In the second case, rods are joined end to end and connected to the same vessels. Let  $q_1$  and  $q_2$  gram per second be the rate of melting of ice in the two cases respectively. The ratio  $\frac{q_1}{q_2}$  is \_\_\_\_\_. (2004)

**Q.7** Three discs, A, B and C having radii  $2\text{m}$ ,  $4\text{m}$  and  $6\text{m}$  respectively are coated with carbon black on their

outer surfaces. The wavelengths corresponding to maximum intensity are  $300 \text{ nm}$ ,  $400 \text{ nm}$  and  $500 \text{ nm}$  respectively. The power radiated by them are  $Q_A$ ,  $Q_B$  and  $Q_C$  respectively. Which is the maximum power radiated? (2004)

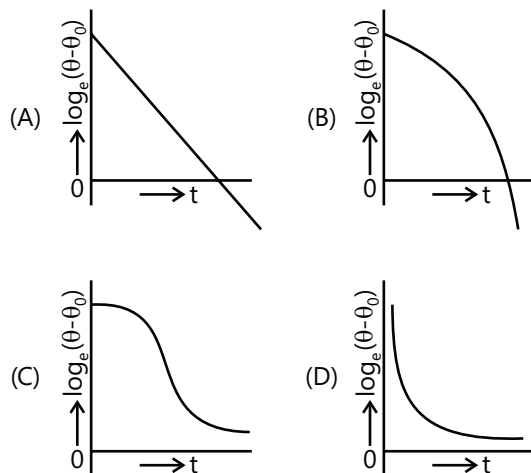
**Q.8** A long metallic bar is carrying heat from one of its ends to the other end under steady-state. The variation of temperature  $\theta$  along the length  $x$  of the bar from its hot end is best described by which of the following figure. (2009)



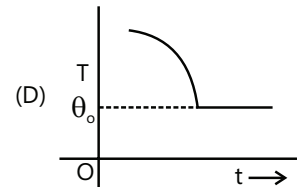
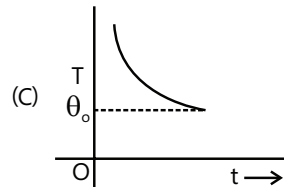
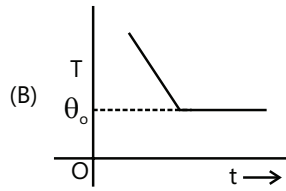
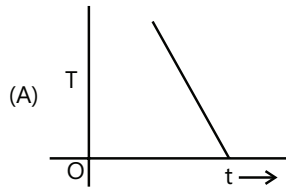
**Q.9**  $100\text{g}$  of water is heated from  $30^\circ\text{C}$  to  $50^\circ\text{C}$ . Ignoring the slight expansion of the water, the change in its internal energy is (specific heat of water is  $4148 \text{ J/kg/K}$ ): (2011)

- (A)  $8.4 \text{ kJ}$  (B)  $84 \text{ kJ}$   
(C)  $2.1 \text{ kJ}$  (D)  $4.2 \text{ kJ}$

**Q.10** A liquid in a beaker has temperature  $\theta(t)$  at time  $t$  and  $\theta_0$  is temperature of surroundings, then according to Newton's law of cooling the correct graph between  $\log_e(\theta - \theta_0)$  and  $t$  is (2012)



**Q.11.** If a piece of metal is heated to temperature  $\theta$  and then allowed to cool in a room which is at temperature  $\theta_0$ , the graph between the temperature  $T$  of the metal and time  $t$  will be closest to: **(2013)**

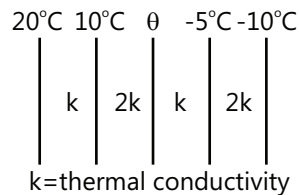


## JEE Advanced/Boards

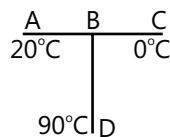
### Exercise 1

**Q.1** A thin walled metal tank of surface area  $5 \text{ m}^2$  is filled with water and contains an immersion heater dissipating  $1 \text{ kW}$ . The tank is covered with  $4 \text{ cm}$  thick layer of insulation whose thermal conductivity is  $0.2 \text{ W/m/K}$ . The outer face of the insulation is  $25^\circ\text{C}$ . Find the temperature of the tank in the steady state.

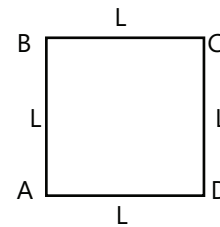
**Q.2** The figure shows the face and interface temperature of a composite slab containing of four layers of two materials having identical thickness. Under steady state condition, find the value of temperature  $\theta$



**Q.3** Three conducting rods of same material and cross-section are shown in figure. Temperature of A, D and C are maintained at  $20^\circ\text{C}$ ,  $90^\circ\text{C}$  and  $0^\circ\text{C}$ . Find the ratio of length BD and BC if there is no heat flow in AB

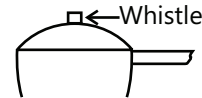


**Q.4** In the square frame of side  $L$  of metallic rods, the corners A and C are maintained at  $T_1$  and  $T_2$  respectively. The rate of heat flow from A to C is  $W$ . If A and D are instead maintained at  $T_1$  and  $T_2$  respectively, find the total rate of heat flow.



**Q.5** One end of copper rod of uniform cross-section and of length  $1.5$  meters is in contact with melting ice and the other end with boiling water. At what point along the length should a temperature of  $200^\circ\text{C}$  be maintained, so that in steady state, the mass of ice melting is equal to that of steam produced in the same interval of time? Assume that the whole system is insulated from the surroundings.

**Q.6** An empty pressure cooker of volume  $10$  liters contains air at atmospheric pressure  $10^5 \text{ Pa}$  and temperature of  $27^\circ\text{C}$ . It contains a whistle which has area of  $0.1 \text{ cm}^2$  and weight of  $100 \text{ gm}$ . What should be temperature of air inside so that the whistle is just lifted up?



### Exercise 2

#### Multiple Correct Choice Type

**Q.1** Two metallic spheres A and B are made of same material and have got identical surface finish. The mass of sphere A is four times that of B. Both the spheres are heated to the same temperature and placed in a room

having lower temperature but thermally insulated from each other.

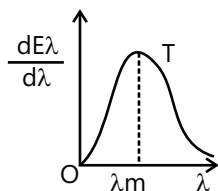
- (A) The ratio of heat loss of A to that of B is  $2^{4/3}$   
 (B) The ratio of heat loss of A to that of B is  $2^{2/3}$   
 (C) The ratio of the initial rate of cooling of A to that of B is  $2^{-2/3}$   
 (D) The ratio of the initial rate of cooling of A to that of B is  $2^{-4/3}$

**Q.2** Two bodies A and B have thermal emissivity of 0.01 and 0.81 respectively. The outer surface areas of the two bodies are the same. The two bodies radiate energy at the same rate. The wavelength  $\lambda_B$ , corresponding to the maximum special radiancy in the radiation from B, is shifted from the wavelength corresponding to the maximum spectral radiancy in the radiation from A by  $1.00 \mu\text{m}$ . If the temperature of A is 5802 K,

- (A) The temperature of B is 1934 K  
 (B)  $\lambda_B = 1.5 \mu\text{m}$   
 (C) The temperature of B is 11604 K  
 (D) The temperature of B is 2901 K

### Comprehension Type

#### Paragraph 1:



**Q.3** The figure shows a radiant energy spectrum graph for a black body at a temperature T.

Choose the correct statement(s)

- (A) The radiant energy is not equally distributed among all the possible wavelengths  
 (B) For a particular wavelength the spectral intensity is maximum  
 (C) The area under the curve is equal to the rate at which heat is radiated by the body at that temperature  
 (D) None of these

**Q.4** If the temperature of the body is raised to higher temperature  $T'$ , then choose the correct statement(s)

- (A) The intensity of radiation for every wavelength increases

(B) The maximum intensity occurs at a shorter wavelength

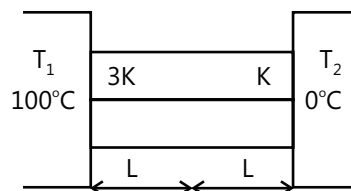
(C) The area under the graph increases

(D) The area under the graph is proportional to the fourth power of temperature

#### Paragraph 2:

Two rods A and B of same cross-sectional area A and length l connected in series between a source ( $T_1 = 100^\circ\text{C}$ ) and a sink ( $T_2 = 0^\circ\text{C}$ ) as shown in figure.

The rod is laterally insulated



**Q.5** The ratio of the thermal resistance of the rod is

- (A)  $\frac{R_A}{R_B} = \frac{1}{3}$  (B)  $\frac{R_A}{R_B} = 3$  (C)  $\frac{R_A}{R_B} = \frac{3}{4}$  (D)  $\frac{4}{3}$

**Q.6** If  $T_A$  and  $T_B$  are the temperature drops across the rod A and B, then

- (A)  $\frac{T_A}{T_B} = \frac{3}{1}$  (B)  $\frac{T_A}{T_B} = \frac{1}{3}$  (C)  $\frac{T_A}{T_B} = \frac{3}{4}$  (D)  $\frac{T_A}{T_B} = \frac{4}{3}$

**Q.7** If  $G_A$  and  $G_B$  are the temperature gradients across the rod A and B, then

- (A)  $\frac{G_A}{G_B} = \frac{3}{1}$  (B)  $\frac{G_A}{G_B} = \frac{1}{3}$  (C)  $\frac{G_A}{G_B} = \frac{3}{4}$  (D)  $\frac{G_A}{G_B} = \frac{4}{3}$

#### Paragraph 3:

In fluids heat transfer takes place and molecules of the medium take very active part. The molecules take energy from high temperature zone and move towards low temperature zone. This method is known as convection, when we require heat transfer with fast phase, we use some mechanism to make the flow of fluid on the body fast. The rate of loss of heat is proportional to velocity of fluid ( $v$ ), and temperature difference ( $\Delta T$ ) between the body and fluid, of course more surface area of body, more rate of loss of heat. We can write the rate of loss of heat as

$$\frac{dQ}{dt} = KAv\Delta T \text{ where } K \text{ is Positive constant.}$$

Now answer the following questions:-

**Q.8** A body is being cooled with fluid. When we increase the velocity of fluid 4 times and decrease the temperature difference  $\frac{1}{2}$  time, the rate of loss of heat increases

- (A) Four times                      (B) Two times  
(C) Six times                        (D) No change

**Q.9** In the above question, if mass of the body increased two times, without change in any of the other parameters, the rate of cooling

- (A) Decreases  
(B) Increases  
(C) No effect of change of mass  
(D) None of these

## Previous Years' Questions

**Q.1** A solid sphere of copper of radius  $R$  and a hollow sphere of the same material of inner radius  $r$  and outer radius  $R$  are heated to the same temperature and allowed to cool in the same environment. Which of them cools faster? **(1982)**

**Q.2** An electric heater is used in a room of total wall area  $137 \text{ m}^2$  to maintain a temperature of  $+20^\circ\text{C}$  inside it, when the outside temperature is  $-10^\circ\text{C}$ . The walls have three different layers. The innermost layer is of wood of thickness  $2.5 \text{ cm}$ , the middle layer is of cement of thickness  $1.0 \text{ cm}$  and the outer most layer is of brick of thickness  $25.0 \text{ cm}$ . Find the power of the electrical heater. Assume that there is no heat loss through the floor and the ceiling. The thermal conductivities of wood, cement and brick are  $0.125$ ,  $1.5$  and  $1.0 \text{ W/m}^\circ\text{C}$  respectively. **(1986)**

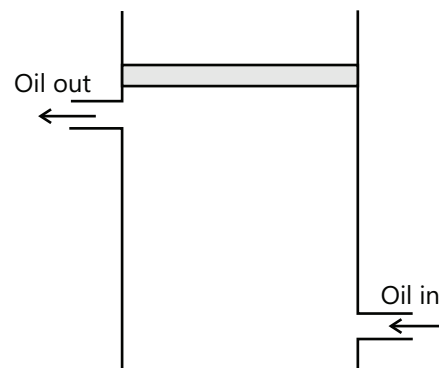
**Q.3** A cylindrical block of length  $0.4 \text{ m}$  and area of cross-section  $0.04 \text{ m}^2$  is placed coaxially on a thin metal disc of mass  $0.4 \text{ kg}$  and of the same cross-section. The upper face of the cylinder is maintained at a constant temperature of  $400\text{K}$  and initial temperature of the disc is  $300\text{K}$ . If the thermal conductivity of the material of the cylinder is  $10\text{W/mK}$  and specific heat capacity of the material of the disc is  $600 \text{ J/kg-K}$ , how long will it take for the temperature of the disc to increase to  $350 \text{ K}$ ? Assume, for purpose of calculation, the thermal conductivity of the disc to be very high and the system to be thermally insulated except for the upper face of the cylinder. **(1992)**

**Q.4** A double-pane window used for insulating a room thermally from outside consists of two glass sheets each of area  $1 \text{ m}^2$  and thickness  $0.01 \text{ m}$  separated by a  $0.05 \text{ m}$  thick stagnant air space. In the steady state, the room glass interface and glass-outdoor interface are at constant temperatures of  $27^\circ\text{C}$  and  $0^\circ\text{C}$  respectively. Calculate the rate of heat of flow through window pane. Also find the temperatures of other interfaces. Given thermal conductivities of glass and air as  $0.8$  and  $0.08 \text{ Wm}^{-1}\text{K}^{-1}$  respectively. **(1997)**

**Q.5** A solid body  $X$  of heat capacity  $C$  is kept in an atmosphere whose temperature is  $T_A = 300 \text{ K}$ . At time  $t=0$ , the temperature of  $X$  is  $T_0 = 400 \text{ K}$ . It cools according to Newton's law of cooling. At time  $t_1$  its temperature is found to be  $350 \text{ K}$ .

At this time ( $t_1$ ), the body  $X$  is connected to a large body  $Y$  at atmospheric temperature  $T_A$  through a conducting rod of length  $L$ , cross-sectional area  $A$  and thermal conductivity  $K$ . The heat capacity of  $Y$  is so large that any variation in its temperature may be neglected. The cross-sectional area  $A$  of the connecting rod is small compared to the surface area of  $X$ . Find the temperature of  $X$  at time  $t = 3t_1$ . **(1998)**

**Q.6** The top of an insulated cylindrical container is covered by a disc having emissivity  $0.6$  and conductivity  $0.167 \text{ W/Km}$  and thickness  $1 \text{ cm}$ . The temperature is maintained by circulating oil as shown



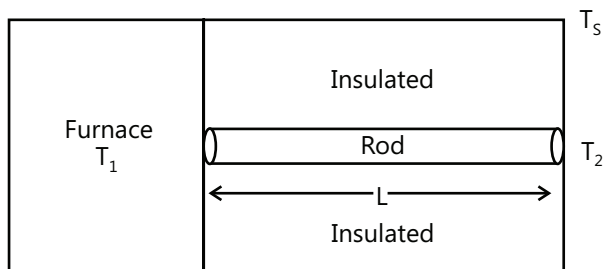
(a) Find the radiation loss to the surroundings in  $\text{W/m}^2$  if temperature of the upper surface of the disc is  $127^\circ\text{C}$  and temperature of surroundings is  $27^\circ\text{C}$ .

(b) Also find the temperature of the circulating oil. Neglect the heat loss due to convection **(2003)**

**Q.7** One end of a rod of length  $L$  and cross-sectional area  $A$  is kept in a furnace of temperature  $T_1$ . The other end of the rod is kept at temperature  $T_2$ . The thermal



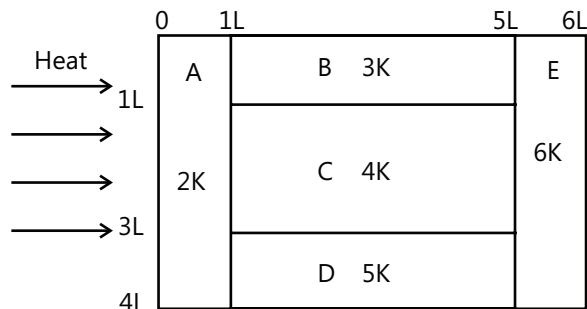
conductivity of the material of the rod is  $K$  and emissivity of the rod is  $e$ .



It is given that  $T_2 = T_s + \Delta T$ , where  $\Delta T \ll T_s$ ,  $T_s$  being the temperature of the surroundings. If  $\Delta T \propto (T_1 - T_s)$ , find the proportionality constant. Consider that heat is lost only by radiation at the end where the temperature of the rod is  $T_2$ . (2004)

**Q.8** Two spherical bodies A (radius 6 cm) and B (radius 18 cm) are at temperatures  $T_1$  and  $T_2$ , respectively. The maximum intensity in the emission spectrum of A is at 500 nm and in that of B is at 1500 nm. Considering them to be black bodies, what will be the ratio of the rate of total energy radiated by A to that of B? (2010)

**Q.9** A composite block is made of slabs A, B, C, D and E of different thermal conductivities (given in terms of a constant  $K$ ) and sizes (given in terms of length,  $L$ ) as shown in the figure. All slabs are of same width. Heat 'Q' flows only from left to right through the blocks. Then in steady state



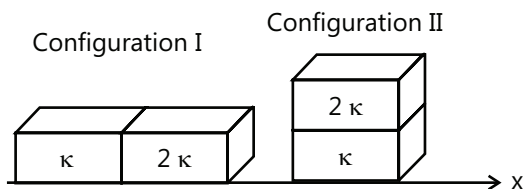
- (A) Heat flow through A and E slabs are same.  
 (B) Heat flow through slab E is maximum.  
 (C) Temperature difference across slab E is smallest.  
 (D) Heat flow through C = heat flow through B + heat flow through D. (2011)

**Q.10** Three very large plates of same area are kept parallel and close to each other. They are considered as ideal black surfaces and have very high thermal conductivity. The first and third plates are maintained at temperatures  $2T$  and  $3T$  respectively. The temperature

of the middle (i.e. second) plate under steady state condition is (2012)

- (A)  $\left(\frac{65}{2}\right)^{1/4} T$  (B)  $\left(\frac{97}{4}\right)^{1/4} T$   
 (C)  $\left(\frac{97}{2}\right)^{1/4} T$  (D)  $(97)^{1/4} T$

**Q.11** Two rectangular blocks, having identical dimensions, can be arranged either in configuration I or in configuration II as shown in the figure. One of the blocks has thermal conductivity  $\kappa$  and the other  $2\kappa$ . The temperature difference between the ends along the x-axis is the same in both the configurations. It takes 9 s to transport a certain amount of heat from the hot end to the cold end in the configuration I. The time to transport the same amount of heat in the configuration II is (2013)



- (A) 2.0 s (B) 3.0 s (C) 4.5 s (D) 6.0

**Q.12** Two spherical stars A and B emit blackbody radiation. The radius of A is 400 times that of B and A emits  $10^4$  times the power emitted from B. The ratio  $(\lambda_A / \lambda_B)$  of their wavelengths  $\lambda_A$  and  $\lambda_B$  at which the peaks occur in their respective radiation curves is (2015)

**Q.13.** A metal is heated in a furnace where a sensor is kept above the metal surface to read the power radiated ( $P$ ) by the metal. The sensor has scale that displays  $\log_2(P/P_0)$ , where  $P_0$  is a constant. When the metal surface is at a temperature of  $487^\circ\text{C}$ , the sensor shows a value 1. Assume that the emissivity of the metallic surface remains constant. What is the value displayed by the sensor when the temperature of the metal surface is raised to  $2767^\circ\text{C}$ ? (2016)

**Q.14** Two moles of ideal helium gas are in a rubber balloon at  $30^\circ\text{C}$ . The balloon is fully expandable and can be assumed to require no energy in its expansion. The temperature of the gas in the balloon is slowly changed to  $35^\circ\text{C}$ . The amount of heat required in raising the temperature is nearly (take  $R = 8.31 \text{ J/mol.K}$ ) (2012)

- (A) 62 J (B) 104 J (C) 124 J (D) 208 J

**Q.15** One mole of mono-atomic ideal gas is taken along two cyclic processes  $E \rightarrow F \rightarrow G \rightarrow E$  and  $E \rightarrow F \rightarrow H \rightarrow E$  as shown in the PV diagram.

The processes involved are purely isochoric, isobaric, isothermal or adiabatic.

Match the paths in list I with the magnitudes of the work done in list II and select the correct answer using the codes given below the lists. **(2013)**

	List I		List II
P.	$G \rightarrow E$	1.	$160 P_0 V_0 \ln 2$
Q.	$G \rightarrow H$	2.	$36 P_0 V_0$
R.	$F \rightarrow H$	3.	$24 P_0 V_0$
S.	$F \rightarrow G$	4.	$31 P_0 V_0$

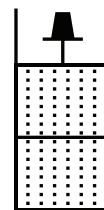
Codes:

- |     |   |   |   |   |
|-----|---|---|---|---|
|     | P | Q | R | S |
| (A) | 4 | 3 | 2 | 1 |
| (B) | 4 | 3 | 1 | 2 |
| (C) | 3 | 1 | 2 | 4 |
| (D) | 1 | 3 | 2 | 4 |

**Paragraph 1:**

In the figure a container is shown to have a movable (without friction) piston on top. The container and the piston are all made of perfectly insulating material

allowing no heat transfer between outside and inside the container. The container is divided into two compartments by a rigid partition made of a thermally conducting material that allows slow transfer of heat. The lower compartment of the container is filled with 2 moles of an ideal monatomic gas at 700 K and the upper compartment is filled with 2 moles of an ideal diatomic gas at 400 K. The heat capacities per mole of an ideal monatomic gas are  $C_V = \frac{3}{2}R, C_P = \frac{5}{2}R$ , and those for an ideal diatomic gas are  $C_V = \frac{5}{2}R, C_P = \frac{7}{2}R$ .



**Q.16** Consider the partition to be rigidly fixed so that it does not move. When equilibrium is achieved, the final temperature of the gases will be **(2014)**

- (A) 550 K    (B) 525 K    (C) 513K    (D) 490 K

**Q.17** Now consider the partition to be free to move without friction so that the pressure of gases in both compartments is the same. Then total work done by the gases till the time they achieve equilibrium will be **(2014)**

- (A) 250 R    (B) 200 R    (C) 100 R    (D) -100 R

## MASTERJEE Essential Questions

### JEE Main/Boards

#### Exercise 1

Q.10      Q.11      Q.12      Q.13

#### Exercise 2

Q.1      Q.2      Q.5      Q.6  
Q.9

### JEE Advanced/Boards

#### Exercise 1

Q.2      Q.3      Q.4      Q.6

#### Exercise 2

Q.1      Q.2      Q.5      Q.6  
Q.7      Q.12      Q.15

## Answer Key

### JEE Main/Boards

#### Exercise 1

**Q.1** Silver is the best conductor of heat

**Q.2** Radiation is the quickest mode of transfer of heat.

**Q.3** The fall in temperature in a body per unit distance is called temperature gradient.

**Q.10**  $3.5 \text{ Wm}^{-1}\text{°C}^{-1}$

**Q.11**  $58.33 \text{ Wm}^{-1}\text{°C}^{-1}$

**Q.12**  $1.587 \text{ gms}^{-1}$

**Q.13** 42 s

**Q.14**  $25\text{°C}$

#### Exercise 2

##### Single Correct Choice Type

**Q.1** A

**Q.2** C

**Q.3** B

**Q.4** A

**Q.5** D

**Q.6** A

**Q.7** C

**Q.8** B

**Q.9** D

#### Previous Years' Questions

**Q.2**  $(1/3)^{1/3}$

**Q.3** 0.69

**Q.4** 1800 W

**Q.5**  $U_2 > U_1$

**Q. 6** 4/1

**Q.7**  $Q_B$

**Q.8** B

**Q.9** A

**Q.10** A

**Q.11** C

### JEE Advanced/Boards

#### Exercise 1

**Q.1**  $65\text{°C}$

**Q.2**  $5\text{°C}$

**Q.3** 7/2

**Q.4**  $(4/3) \text{ W}$

**Q.5** 10.34 cm

**Q.6**  $327\text{°C}$

#### Exercise 2

##### Multiple Correct Choice Type

**Q.1** A, C

**Q.2** A, B

##### Comprehension Type

**Paragraph 1:** **Q.3** A, B

**Q.4** A, B, C, D

**Paragraph 2:** **Q.5** A

**Q.6** B

**Q.7** B

**Paragraph 3:** **Q.8** B

**Q.9** A

## Previous Years' Questions

**Q.1** Hollow Sphere

**Q.2** 9091 W

**Q.3**  $T=166.32$  s

**Q.4** 41.6 W, 26.48 °C, 0.52 °C

**Q.5**  $T_2 = \left( 300 + 12.5e^{\frac{-2AKt_1}{CL}} \right)$

**Q.6** (a) 595 W/m<sup>2</sup>, (b) 162.6°C

**Q.7**  $\frac{K}{4\epsilon\sigma L T_c^3 + K}$

**Q.8** 9

**Q.9**: A, C, D or A, B, C, D

**Q.10** C

**Q.11** A

**Q.12** 2

**Q.13** 9

**Q.14** D

**Q.15** A

**Q.16** D

**Q.17** D

## Solutions

### JEE Main/Boards

#### Exercise 1

**Sol 1:** Silver is the best conductor of heat

**Sol 2:** Radiation

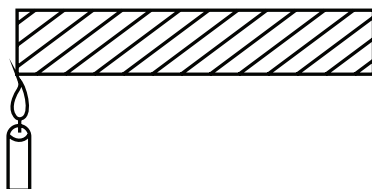
**Sol 3:** Temperature gradient → Fall in temperature in a body per unit distance is called the temperature gradient.

**Sol 4:** Three Methods:

- (i) Conduction
- (ii) Convection
- (iii) Radiation – fastest one because heat travels without any intervening medium.

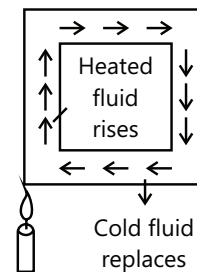
**Sol 5:** Conduction:- Heat flows from a place of higher temperature to a place of lower temperature with the medium remaining stationary.

Eg. A metal rod heated from one end



Convection: When a fluid in a vessel is heated, lighter molecules present in the lower layer of the fluid get heated, which rise and cold molecules go to the bottom of the vessel. i.e. by movement of the molecules of fluid.

E.g. A gas vessel filled with fluid being heated from bottom.



Radiation:- Heat travels directly from one place to another without any intervening medium.

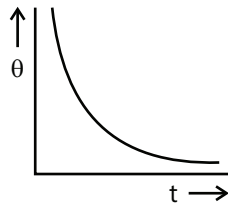
E.g. Heat from the sun to the earth.

**Sol 6:** Thermal radiations are electromagnetic waves which are invisible. These are radiated from a heated surface in all directions. These travel with velocity of light in a straight line and does not require an intervening medium to carry it.

**Sol 7:** If a body at temperature  $\theta_1$  is placed in surroundings at lower temperature  $\theta_2$ , then it is observed that magnitude of temperature gradient decreases with time

i.e.  $-\frac{d\theta}{dt} \propto (\theta - \theta_2)$  [Newton's law of cooling]

$\Rightarrow \frac{d\theta}{dt} = -k(\theta - \theta_2)$   $k \rightarrow$  a constant



**Sol 8:** Thermal conductivity is the property of a material to conduct heat.

Coefficient of thermal conductivity ( $k$ ) is the measure of thermal conductivity which is equal to the quantity of heat flowing per unit time through area of cross-section of a material per unit length along the direction of flow of heat.

S.I. Units: -  $\text{J}\cdot\text{m}^{-1}\text{sec}^{-1}\text{K}^{-1}$

C.G.S. Units: -  $\text{cal}\cdot\text{cm}^{-1}(\text{C}^{\circ})^{-1}$

**Sol 9:** The rate of cooling of a body is directly proportional to the difference of temperature of the body over its surrounding.

Body temperature at any time 't'  $\rightarrow \theta$

Body initial temperature  $\rightarrow \theta_1$

Surrounding temperature  $\rightarrow \theta_2$

$\therefore$  Rate of cooling i.e.  $\frac{-dQ}{dt} \propto (\theta - \theta_2)$

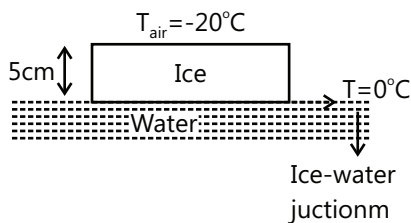
$$\therefore \frac{dQ}{dt} = -k(\theta - \theta_2)$$

$$\Rightarrow ms \frac{d\theta}{dt} = -k(\theta - \theta_2)$$

$$\Rightarrow \frac{d\theta}{dt} = -\left(\frac{k}{ms}\right)(\theta - \theta_2)$$

**Sol 10:**  $\frac{dQ}{dt} = 20000 \text{ cal min}^{-1}$

$$= \frac{20000 \times 4.2}{60} \text{ J sec}^{-1}$$



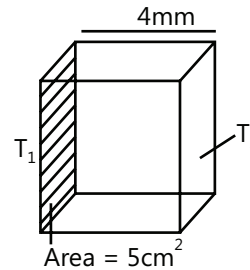
$$\Rightarrow \frac{-K\Delta\theta}{\Delta x} = \frac{20000 \times 4.2}{60}$$

$$\Rightarrow \frac{-K[(-20) - (0)]}{5/100} = 1400 \Rightarrow K = 3.5 \text{ Wm}^{-1}\text{C}^{\circ}$$

**Sol 11:**  $\ell = 4\text{mm} = 4 \times 10^{-3} \text{ m}$

$$\Delta T = 32^{\circ} \text{ C}$$

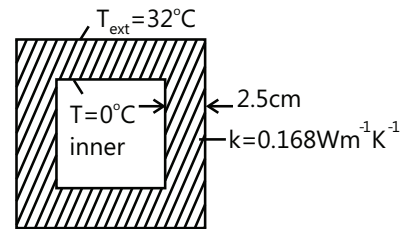
$$\frac{dQ}{dt} = 200 \text{ kcal h}^{-1} \approx 233.33 \text{ J/sec}$$



$$\Rightarrow \frac{KA\Delta T}{\ell} = 233.33 \text{ J/sec}$$

$$\Rightarrow K = \frac{233.33 \times 4 \times 10^{-3}}{32 \times 5 \times 10^{-4}} = 58.33 \text{ J/m }^{\circ}\text{C sec}$$

**Sol 12:** Area of surface perpendicular to direction of flow of heat  $\approx$  surface area of inner rectangle



$$\approx [2 [100 \times 60] + 2 [60 \times 40] + 2 [100 \times 40]] \times 10^{-4}$$

$$= 2.48 \text{ m}^2$$

$$\therefore \frac{dQ}{dt} = \frac{-kA}{\ell} (T_{\text{ext}} - T_{\text{inner}})$$

$$= -\frac{0.168 \times 2.48 \times 32}{2.5 \times 10^{-2}} = -533.29 \text{ J/sec}$$

Therefore, rate at which ice melts

$$= \frac{533.29}{80 \times 4.2} \text{ gm/sec} = 1.587 \text{ gm/sec}$$

**Sol 13:**  $T = T_{\text{surrounding}} + (T_{\text{initial}} - T_{\text{surrounding}}) e^{-kt}$

$$\Rightarrow \ln\left(\frac{T - T_{\text{surrounding}}}{T_{\text{initial}} - T_{\text{surrounding}}}\right) = -kt$$

Let when  $t = 0$ ,  $T_{\text{initial}} = 94^{\circ}\text{C}$ ,  $T_{\text{surrounding}} = 20^{\circ}\text{C}$

$$\therefore -k \times 2 = \ln\left(\frac{86 - 20}{94 - 20}\right)$$

$$\Rightarrow -2k = \ln\left(\frac{66}{74}\right) \Rightarrow -k = \frac{-0.114}{2}$$

and let  $t = 0$  when,  $T_{\text{initial}} = 71^\circ\text{C}$

$$\therefore -kt = \ln\left(\frac{69-20}{71-20}\right) = \ln\left(\frac{49}{51}\right)$$

$$\Rightarrow t \approx 0.70 \text{ min} = 42 \text{ sec}$$

**Sol 14:**  $T_i = 70^\circ\text{C}$

$$T_f = 55^\circ\text{C} \rightarrow t = 5 \text{ min}$$

$$T'_f = 45^\circ\text{C} \rightarrow t' = 10 \text{ min}$$

$T_0 \rightarrow$  Temperature of surrounding

$\therefore$  From Newton's law

$$T - T_0 = (T_i - T_0) e^{-kt}$$

We have following equation.

$$\Rightarrow 55 - T_0 = (70 - T_0) e^{-5k}$$

$$\text{And } 45 - T_0 = (70 - T_0) e^{-10k}$$

Dividing equations (ii)/(i)

$$\Rightarrow \frac{45 - T_0}{55 - T_0} = e^{-5k}$$

Substitute value of  $e^{-5k}$  in (i)

$$\Rightarrow (55 - T_0) = (70 - T_0) \left(\frac{45 - T_0}{55 - T_0}\right)$$

$$\Rightarrow \frac{55 - T_0}{70 - T_0} - 1 = \frac{45 - T_0}{55 - T_0} - 1$$

$$\Rightarrow \frac{-15}{70 - T_0} = \frac{-10}{55 - T_0}$$

$$\Rightarrow T_0 = 25^\circ\text{C}$$

## Exercise 2

### Single Correct Choice Type

**Sol 1: (A)**  $\frac{dQ}{dt} = -\frac{kA}{L} \Delta T$

The greater the value of  $\frac{A}{L}$ , more the heat will be conducted.

(A)  $\frac{A}{L} = \frac{\pi(2)^2}{0.5} = 8\pi$

(B)  $\frac{A}{L} = 2\pi$

(C)  $\frac{A}{L} = \frac{\pi}{2}$

(D)  $\frac{A}{L} = \pi$

Therefore (A) will conduct more heat.

**Sol 2: (C)**  $\left(\frac{dQ}{dt}\right)_{\text{across A}} = \left(\frac{dQ}{dt}\right)_{\text{across B}}$

$$\Rightarrow \frac{-(2k) \times A}{\ell} \Delta T_A = \frac{-(k) \times A}{\ell} \times 36$$

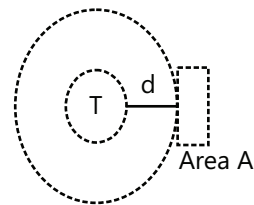
$$\Rightarrow \Delta T_A = 18^\circ\text{C}$$

$$\left| \begin{array}{c|c} A & B \\ \hline 2k & k \\ \hline -\ell & -\ell \end{array} \right|$$

... (i)

... (ii)

**Sol 3: (B)**  $P = \text{Area of foil} \times \text{Intensity } (A_{\text{foil}})$



$$\text{Intensity} = \frac{\text{Power emitted}}{\text{Area of sphere}} = \frac{eA\sigma T^4}{4\pi d^2}$$

$$\therefore P = A_{\text{foil}} \times \frac{eA\sigma T^4}{4\pi d^2}$$

When temperature and distance are double

$$\therefore P' = A_{\text{foil}} \times \frac{eA\sigma(2T)^4}{4\pi(2d)^2} = 4P$$

**Sol 4: (A)** At  $T = 273^\circ\text{C} = (273 + 273) \text{ K}$

$$E = eA\sigma (273 + 273)^4 = 16eA\sigma (273)^4$$

$$\text{At } T = 273 \text{ K; } E' = eA\sigma (273)^4 = \frac{E}{16}$$

$$\therefore E' = \frac{E}{16}$$

**Sol 5: (D)**  $\lambda_m T = \text{const.} = 2.93 \times 10^{-3} \text{ mK}$

$$P = eA\sigma T^4$$

Given:  $\lambda_0 T = \text{const.} = c$  (say)

$$\text{When } \lambda_m = \frac{3}{4} \lambda_0 \text{ then } \frac{3}{4} \lambda_0 \times T' = c$$

$$\Rightarrow T' = \frac{4}{3} T$$

$$\therefore P' = eA\sigma \left(\frac{4}{3}T\right)^4$$

$$\Rightarrow P' = \frac{256}{81} P$$

**Sol 6: (A)** By Wien's displacement law:-

$$\lambda_m T = \text{constant} = C$$

$$\therefore \lambda_{m1} T_1 = \lambda_{m2} T_2$$

$$\Rightarrow 420 T_1 = 560 T_2$$

$$\Rightarrow \frac{T_1}{T_2} = \frac{560}{420} = \frac{4}{3}$$

**Sol 7: (C)**  $r_\theta = 3r_p$

$$P = eA\sigma T^4$$

$$\Rightarrow mc \frac{dT}{dt} = eA\sigma T^4$$

(c: specific heat, m: mass of sphere)

$$\Rightarrow \frac{dT}{dt} = \frac{-eA\sigma T^4}{mc} = \frac{-eA\sigma T^4}{(\rho V)c} = \frac{-e4\pi r^2 \sigma T^4}{\frac{4}{3}\pi r^3 c}$$

(V: volume of sphere)

$$\Rightarrow \frac{dT}{dt} = \frac{1}{r} \times \left[ \frac{-3e\sigma T^4}{c} \right]$$

[Quantity in parenthesis is Constant for both spheres]

$$\therefore \frac{\left(\frac{dT}{dt}\right)_P}{\left(\frac{dT}{dt}\right)_Q} = \frac{\frac{1}{r_P}}{\frac{1}{r_Q}} = 3 = x$$

**Sol 8: (B)** By Newton's law of cooling:-

$$(T - T_a) = (T_0 - T_a) e^{-kt}$$

$T_a$ : Surrounding temperature

$T_0$ : Initial temperature

When  $T_0 = 60^\circ \text{C}$ ,  $T = 50^\circ \text{C}$ ,  $t = 4 \text{ min}$

$$\therefore (50 - T_a) = (60 - T_a) e^{-4k} \quad \dots(i)$$

When  $T_0 = 40$ ,  $T = 30$  then  $t = 8 \text{ min}$

$$\therefore (30 - T_a) = (40 - T_a) e^{-8k} \quad \dots(ii)$$

Dividing (ii)/(i) gives

$$\frac{30 - T_a}{50 - T_a} = \frac{40 - T_a}{60 - T_a} e^{-4k} \quad \dots(iii)$$

On substituting value of  $e^{-4k}$  from (i) into (iii) we get:

$$\frac{30 - T_a}{50 - T_a} = \frac{40 - T_a}{60 - T_a} \times \left( \frac{50 - T_a}{60 - T_a} \right)$$

$$\Rightarrow (30 - T_a)(60 - T_a)^2 = (40 - T_a)(50 - T_a)^2$$

$$\Rightarrow (T_a - 60)(T_a - 60)(T_a - 30) = (T_a - 50)(T_a - 50)(T_a - 40)$$

$$\Rightarrow T_a^3 - [60 + 60 + 30]T_a^2 + [60 \times 60 + 60 \times 30 + 60 \times 30]T_a - 60 \times 60 \times 30 = T_a^3 - [50 + 50 + 40]T_a^2 + [50 \times 50 + 50 \times 40 + 50 \times 40]T_a - 50 \times 50 \times 40$$

$$\Rightarrow -10T_a^2 + 700T_a - 8000 = 0$$

$$\Rightarrow T_a^2 - 70T_a + 800 = 0$$

$$\Rightarrow T_a = 55.61 \text{ or } 14.38$$

**Sol 9: (D)**  $P = \frac{dQ}{dt} = S \times \frac{d\theta}{dt} = k(\theta_1 - \theta_0)$

$$10 \text{ W} = k(50 - 20) \quad k = \frac{10 \text{ W}}{30^\circ \text{C}}$$

$$S \times \frac{d\theta}{dt} = k(\theta - \theta_0)$$

$$\Rightarrow S \frac{\Delta\theta}{\Delta t} = k(\theta - \theta_0) \quad \theta = \frac{35.1 + 34.9}{2} = 35$$

$$S \left( \frac{0.2}{60 \text{ sec}} \right) = \frac{10}{30} (35 - 20)$$

$$S = 1500 \text{ J / } ^\circ \text{C}$$

## Previous Years' Questions

**Sol 1:** Let  $R_1$  and  $R_2$  be the thermal resistances of inner and outer portions. Since, temperature difference at both ends is same, the resistances are in parallel. Hence,

$$\frac{1}{R} = \frac{1}{R_1} + \frac{1}{R_2}$$

$$\therefore \frac{K(4\pi R^2)}{\ell} = \frac{K_1(\pi R^2)}{\ell} + \frac{K_2(3\pi R^2)}{\ell}$$

$$\therefore K = \frac{3K_2 + K_1}{4}$$



**Sol 2:** The rate at which energy radiates from the object is

$$\frac{\Delta Q}{\Delta t} = e\sigma AT^4$$

Since,  $\Delta Q = mc\Delta T$ , we get

$$\frac{\Delta T}{\Delta t} = \frac{e\sigma AT^4}{mc}$$

Also, since  $m = \frac{4}{3}\pi r^3\rho$  for a sphere, we get

$$A = 4\pi r^2 = 4\pi \left(\frac{3m}{4\pi\rho}\right)^{2/3}$$

$$\text{Hence, } \frac{\Delta T}{\Delta t} = \frac{e\sigma T^4}{mc} \left[4\pi \left(\frac{3m}{4\pi\rho}\right)^{2/3}\right] = K \left(\frac{1}{m}\right)^{1/3}$$

For the given two bodies

$$\frac{(\Delta T / \Delta t)_1}{(\Delta T / \Delta t)_2} = \left(\frac{m_2}{m_1}\right)^{1/3} = \left(\frac{1}{3}\right)^{1/3}$$

**Sol 3:** From Wien's displacement law

$$\lambda_m T = \text{constant}$$

$$\text{or } T = \frac{1}{\lambda_m}$$

$$\therefore \frac{T_{\text{sun}}}{T_{\text{northstar}}} = \frac{(\lambda_m)_{\text{north star}}}{(\lambda_m)_{\text{sun}}} = \frac{350}{510} \approx 0.69$$

**Sol 4:** Power radiated  $\propto$  (surface area)( $T$ )<sup>4</sup>. The radius is halved, hence, surface area will become  $\frac{1}{4}$  times. Temperature is doubled, therefore,  $T^4$  becomes 16 times.

$$\text{New power} = (450) \left(\frac{1}{4}\right) (16) = 1800 \text{ W.}$$

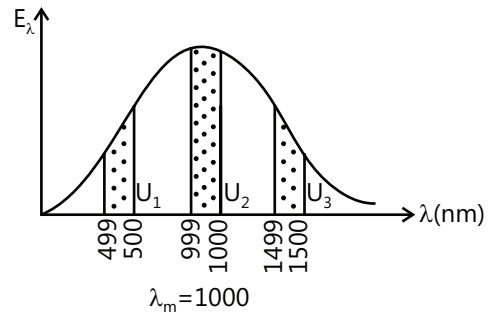
**Sol 5:** Wien's displacement law is

$$\lambda_m T = b \quad (b = \text{Wien's constant})$$

$$\therefore \lambda_m = \frac{b}{T} = \frac{2.88 \times 10^6 \text{ nm-K}}{2880 \text{ K}}$$

$$\therefore \lambda = 1000 \text{ nm}$$

Energy distribution with wavelength will be as follows:



From the graph it is clear that

$U_2 > U_1$  (In fact  $U_2$  is maximum)

$$\text{Sol 6: } q = \frac{dm}{dt} \propto \frac{1}{\text{Thermal Resistance}}$$

In the first case rods are in parallel and thermal resistance is  $\frac{R}{2}$  while in second case rods are in series and thermal resistance is  $2R$ .

$$\frac{q_1}{q_2} = \frac{2R}{R/2} = \frac{4}{1}$$

**Sol 7:**  $Q \propto AT^4$  and  $\lambda_m T = \text{constant}$ .

$$\text{Hence, } Q \propto \frac{A}{(\lambda_m)^4} \text{ or } Q \propto \frac{r^2}{(\lambda_m)^4}$$

$$Q_A : Q_B : Q_C = \frac{(2)^2}{(3)^4} : \frac{(4)^2}{(4)^4} : \frac{(6)^2}{(5)^4}$$

$$= \frac{4}{81} : \frac{1}{16} : \frac{36}{625}$$

$$= 0.05 : 0.0625 : 0.0576$$

i.e.,  $Q_B$  is maximum.

**Sol 8: (B)** We know that  $\frac{dQ}{dt} = kA \frac{d\theta}{dx}$

In steady state flow of heat

$$d\theta = \frac{dQ}{dt} \cdot \frac{1}{kA} dx$$

$$\Rightarrow \theta_H - \theta = kx' \Rightarrow \theta = \theta_H - kx'$$

Equation  $\theta = \theta_H - k'x$  represents a straight line.

**Sol 9: (A)**  $\Delta Q = \Delta U + \Delta W$  (ignoring expansion)

$$\Delta U = ms\Delta T = 0.1 \times 4.184 \times 20 = 8.368 \text{ kJ}$$



**Sol 10: (A)** According to Newtons law of cooling.

$$\frac{d\theta}{dx} \propto (\theta - \theta_0)$$

$$\Rightarrow \frac{d\theta}{dt} = -k(\theta - \theta_0)$$

$$\int \frac{d\theta}{\theta - \theta_0} = \int -k dt$$

$$\Rightarrow \ln(\theta - \theta_0) = -kt + c$$

Hence the plot of  $\ln(\theta - \theta_0)$  vs  $t$  should be a straight line with negative slope.

**Sol 11: (C)** According to Newtons cooling law, option C is the correct option.

## JEE Advanced/Boards

### Exercise 1

**Sol 1:** Continuously 1 kW of heat is being dissipated from 25°C tank.

$$\therefore \frac{dQ}{dt} = 10^3 = \frac{-KA[25 - T]}{l}$$

$$\Rightarrow \frac{dQ}{dt} = 10^3 = \frac{-0.2 \times 5 \times [25 - T]}{4 \times 10^{-2}}$$

$$\Rightarrow 25 - T = -40 ; \Rightarrow T = 65^\circ\text{C}$$

**Sol 2:** For 1<sup>st</sup> layer

$$\frac{dQ}{dt} = \frac{-KA\Delta T}{l} = \frac{-KA(10 - 20)}{l} = \frac{+KA \times 10}{l}$$

For 2<sup>nd</sup> layer

$$\frac{dQ}{dt} = \frac{-(2k)A(\theta - 10)}{l} = \frac{-2AK}{l} [\theta - 10]$$

Rate for both layers must be equal

$$\therefore \frac{kA \times 10}{l} = \frac{-2kA}{l} (\theta - 10) ; \Rightarrow \theta = 5^\circ\text{C}$$

**Sol 3:** If  $\left(\frac{dQ}{dt}\right)_{AB} = 0$

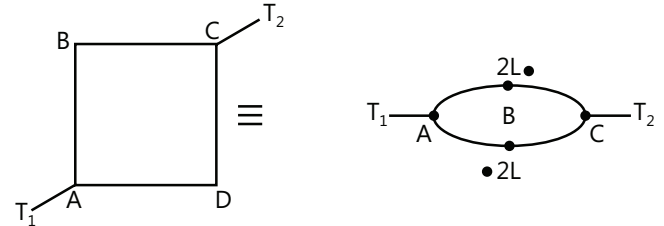
Then rate of heat flow from D to B must be equal to rate of heat flow from B to C.

$$\text{i.e. } \left(\frac{dQ}{dt}\right)_{DB} = \left(\frac{dQ}{dt}\right)_{BC}$$

$$\Rightarrow -\frac{kA(T_B - T_D)}{l_{DB}} = \frac{-kA(T_C - T_B)}{l_{BC}}$$

$$\Rightarrow \frac{(20 - 90)}{l_{DB}} = \frac{(0 - 20)}{l_{BC}} ; \Rightarrow \frac{l_{BD}}{l_{BC}} = \frac{-70}{-20} = 3.5$$

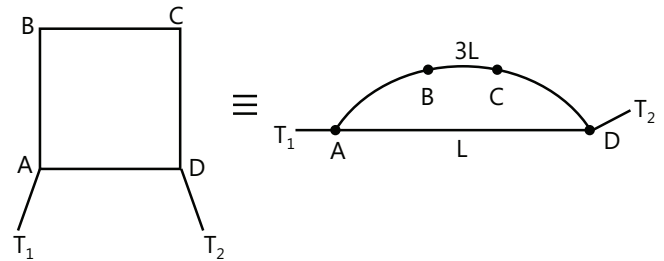
**Sol 4:**



$$\therefore \left(\frac{dQ}{dt}\right)_{AC} = \left(\frac{dQ}{dt}\right)_{ABC} + \left(\frac{dQ}{dt}\right)_{ADC}$$

$$\Rightarrow W = \frac{-kA(T_2 - T_1)}{2L} + \frac{-kA(T_2 - T_1)}{2L}$$

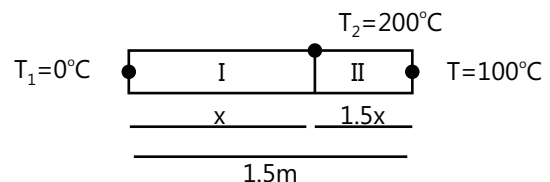
$$\Rightarrow W = \frac{-kA(T_2 - T_1)}{L}$$



$$\therefore \left(\frac{dQ}{dt}\right)_{AD} = \frac{-kA(T_2 - T_1)}{3L} + \frac{-kA(T_2 - T_1)}{L}$$

$$= \frac{-4kA(T_2 - T_1)}{L} = \frac{4}{3} W$$

**Sol 5:**



Mass of ice melting per second = mass of steam produced per sec

$$\Rightarrow \frac{-kA(0 - 200)}{80} = \frac{-kA(100 - 200)}{540}$$

$$\Rightarrow \frac{1.5-x}{x} = \frac{1}{2} \times \frac{80}{540}$$

$$\Rightarrow x = \frac{27 \times 1.5}{29} \approx 1.3966 \text{ m}$$

$$\therefore 1.5 - x = 0.1034 \text{ m} = 10.34 \text{ cm}$$

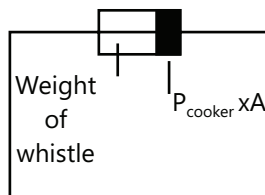
**Sol 6:** Mass of whistle = 100 gm = 0.1 kg

$$\therefore \text{Weight of whistle} = 1 \text{ N}$$

To just lift the whistle, pressure in pressure cooker must be equal to = Atmospheric pressure + Pressure due to weight of whistle

$$= 10^5 + \frac{1\text{N}}{0.1 \times 10^{-4} \text{m}^2} = 2 \times 10^5 \text{ Pa}$$

Free-body diagram of whistle  $P_{\text{atm}} A$



By Force-balance

$$P_{\text{atm}} \times A + \text{weight of whistle} = P_{\text{cooker}} \times A$$

$$\Rightarrow P_{\text{cooker}} = P_{\text{atm}} + \frac{\text{weight of whistle}}{A}$$

Initially, it is given  $P = 10^5 \text{ Pa}$ ,  $V = 10 \text{ L}$ ,  $T = 300\text{K}$

$$\therefore P.V. = nRT; \Rightarrow nR = \frac{10 \times 10^5}{300} \text{ Pa.L/K} \quad \dots(i)$$

Finally, we require  $P = 2 \times 10^5 \text{ Pa}$ ,  $V = 10 \text{ L}$ ,  $T = ?$

$\therefore$  By gas equation:-  $PV = nRT$

$$\Rightarrow 2 \times 10^5 \times 10 = \frac{10 \times 10^5}{300} \times T \text{ [using (i)]}$$

$$\Rightarrow T = 600 \text{ K} = 327^\circ \text{C}$$

## Exercise 2

### Multiple Correct Choice Type

**Sol 1: (A, C)**  $\rho = \frac{m}{V}$

$$\Rightarrow \rho \times \frac{4}{3} \pi r^3 = m; \Rightarrow r \propto (m)^{1/3}$$

and Area of sphere  $(A) \propto r^2$

$$\therefore A \propto (m)^{2/3}$$

$$\therefore \frac{A_A}{A_B} = (4)^{2/3} = (2)^{4/3}$$

$$\therefore \text{Ratio of heat loss} = \frac{eA_A \sigma (T - T_0)^4}{eA_B \sigma (T - T_0)^4} = \frac{A_A}{A_B} = (2)^{4/3}$$

By Newton's law of cooling:

$$\frac{dQ}{dt} = ms \frac{dT}{dt} = -k(T - T_0)$$

$$\Rightarrow \frac{dT}{dt} = \frac{-k}{ms} (T - T_0)$$

where  $k = 4e A \sigma T_0^3$

$$\therefore \frac{dT}{dt} \propto \frac{A}{m}$$

$$\therefore \frac{\left(\frac{dT}{dt}\right)_A}{\left(\frac{dT}{dt}\right)_B} = \frac{\frac{A_A}{m_A}}{\frac{A_B}{m_B}} = \frac{(2)^{4/3}}{4} = 2^{-2/3}$$

**Sol 2: (A, B)**  $e_A = 0.01$  and  $e_B = 0.81$

$$A_A = A_B$$

$$E_A = E_B$$

$$\Rightarrow e_A \sigma A_A T_A^4 = e_B \sigma A_B T_B^4$$

$$\Rightarrow 0.01 T_A^4 = 0.81 T_B^4$$

$$\Rightarrow T_B = \frac{1}{3} \times T_A$$

$$\Rightarrow T_B = \frac{1}{3} \times 5802 = 1934 \text{ K}$$

By Wien's displacement law

$$\lambda_m T = \text{const.} = 2.93 \times 10^{-3} \text{ mK}$$

$$\therefore \lambda_{m_A} = 0.5 \mu\text{m}$$

Since, it is given in the question that

$$\lambda_{m_B} = 1 \mu\text{m} + \lambda_{m_A}$$

$$\therefore \lambda_{m_B} = 1.5 \mu\text{m}$$

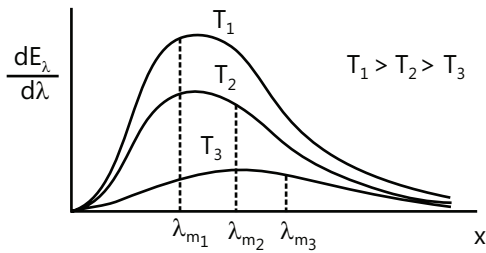
### Comprehension Type

#### Paragraph 1

**Sol 3: (A, B)** Area under the curve gives the rate at which heat per unit surface is radiated by the body i.e. total rate of heat radiation = (Area under the curve)  $\times$  (surface area of the body)

**Sol 4: (A, B, C, D)**  $\lambda_m T = \text{const.}$  [By Wien's displacement law]

Area under graph =  $E_\lambda = e \sigma T^4 \propto T^4$



### Paragraph 2

**Sol 5: (A)**  $A_A = A$  ;  $A_B = A$

$\ell_A = l$  ;  $\ell_B = l$

$k_A = 3k$  ;  $k_B = k$

$$\therefore R_A = \frac{\ell_A}{k_A A_A} = \frac{\ell}{3kA} ; \quad R_B = \frac{\ell_B}{k_B A_B} = \frac{\ell}{kA}$$

$$\therefore \frac{R_A}{R_B} = \frac{1}{3}$$

**Sol 6: (B)** Rate at which heat flows from A

= Rate at which heat flows from B

$$\Rightarrow \left( \frac{dQ}{dt} \right)_A = \left( \frac{dQ}{dt} \right)_B$$

$$\Rightarrow \frac{T_A}{R_A} = \frac{T_B}{R_B} \Rightarrow \frac{T_A}{T_B} = \frac{R_A}{R_B} = \frac{1}{3}$$

**Sol 7: (B)**  $G_A = \frac{T_A}{L_A} = \frac{T_A}{L}$  and  $G_B = \frac{T_B}{L_B} = \frac{T_B}{L}$

$$\therefore \frac{G}{G_B} = \frac{T_A}{T_B} = \frac{1}{3}$$

### Paragraph 3

**Sol 8: (B)**  $\left( \frac{dQ}{dt} \right)_{\text{initially}} = KA v \Delta T$

$$\left( \frac{dQ}{dt} \right)_{\text{finally}} = KA(4v) \left( \frac{\Delta T}{2} \right) = 2 \left( \frac{dQ}{dt} \right)_{\text{initially}}$$

**Sol 9: (A)** If all the parameters are kept constant then

$$\frac{dQ}{dt} = ms \frac{dT}{dt} = kA v \Delta T$$

$$\therefore \frac{dT}{dt} = \frac{kAv\Delta T}{ms}$$

## Previous Years' Questions

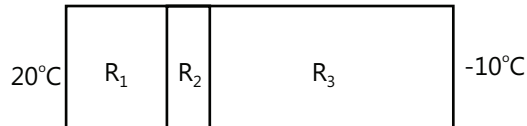
**Sol 1:** Net rate of heat radiation  $\left( \frac{dQ}{dt} \right)$  will be same in both the cases, as temperature and area are same.

Therefore, from equation

$$ms \left( -\frac{d\theta}{dt} \right) = \frac{dQ}{dt} \text{ or } -\frac{d\theta}{dt} \propto \frac{1}{m}$$

The hollow sphere will cool faster as its mass is less.

**Sol 2:** Let  $R_1$ ,  $R_2$  and  $R_3$  be the thermal resistances of wood, cement and brick. All the resistances are in series. Hence,



$$R = R_1 + R_2 + R_3$$

$$= \frac{2.5 \times 10^{-2}}{0.125 \times 137} + \frac{1.0 \times 10^{-2}}{1.5 \times 137} + \frac{25 \times 10^{-2}}{1.0 \times 137}$$

$$= 0.33 \times 10^{-2} \text{ } ^\circ\text{C/W} \quad \left( \text{as } R = \frac{\ell}{KA} \right)$$

$\therefore$  Rate of heat transfer,

$$\frac{dQ}{dt} = \frac{\text{Temperature difference}}{\text{thermal resistance}} = \frac{30}{0.33 \times 10^{-2}}$$

$$\approx 9091 \text{ W}$$

$\therefore$  Power of heater should be 9091 W.

**Sol 3:** Let at any time temperature of the disc be  $\theta$ .

At this moment rate of heat flow,

$$\frac{dQ}{dt} = \frac{KA(\Delta\theta)}{\ell} = \frac{KA}{\ell} (\theta_0 - \theta) \quad \dots (i)$$

This heat is utilised in increasing the temperature of the disc.

$$\text{Hence, } \frac{dQ}{dt} = ms \frac{d\theta}{dt} \quad \dots (ii)$$

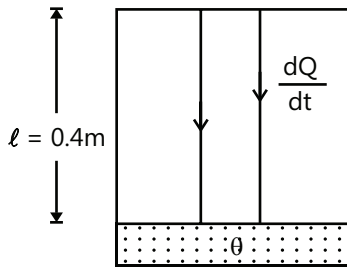
Equating Eqs. (i) and (ii), we have

$$ms \frac{d\theta}{dt} = \frac{KA}{\ell} (\theta_0 - \theta)$$

$$\text{Therefore, } \frac{d\theta}{\theta_0 - \theta} = \frac{KA}{ms\ell} dt$$

$$\text{or } \int_{300K}^{350K} \frac{d\theta}{\theta_0 - \theta} = \frac{KA}{ms\ell} \int_0^t dt$$

$$\text{or } [-\ln(\theta_0 - \theta)]_{300K}^{350K} = \frac{KA}{ms\ell} t$$



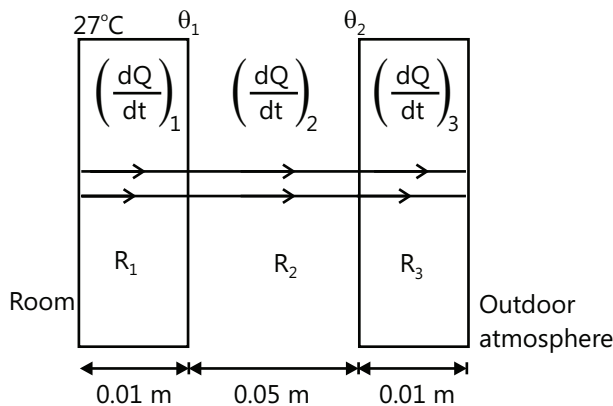
$$\therefore t = \frac{ms\ell}{KA} \lambda n \left( \frac{\theta_0 - 300}{\theta_0 - 350} \right)$$

Substituting the values, we have

$$T = \frac{(0.4)(600)(0.4)}{(10)(0.04)} \ln \left( \frac{400 - 300}{400 - 350} \right)$$

$$T = 166.32 \text{ s}$$

**Sol 4:** Let  $\theta_1$  and  $\theta_2$  be the temperatures of the two interfaces as shown in figure.



$$\text{Thermal resistance, } R = \frac{\ell}{KA}$$

$$\therefore R_1 = R_3 = \frac{(0.01)}{(0.8)(1)} = 0.0125 \text{ K/W or } ^\circ\text{C/W}$$

$$\text{and } R_2 = \frac{(0.05)}{(0.08)(1)} = 0.625 \text{ } ^\circ\text{C/W}$$

Now the rate of heat flow  $\left( \frac{dQ}{dt} \right)$  will be equal from all the three sections and since rate of heat flow is given by

$$\frac{dQ}{dt} = \frac{\text{Temperature difference}}{\text{Thermal resistance}}$$

$$\text{and } \left( \frac{dQ}{dt} \right)_1 = \left( \frac{dQ}{dt} \right)_2 = \left( \frac{dQ}{dt} \right)_3$$

$$\text{Therefore, } \frac{27 - \theta_1}{0.0125} = \frac{\theta_1 - \theta_2}{0.625} = \frac{\theta_2 - \theta}{0.0125}$$

Solving this equation, we get

$$\theta_1 = 26.48^\circ\text{C}$$

$$\text{and } \theta_2 = 0.52^\circ\text{C}$$

$$\text{and } \frac{dQ}{dt} = \frac{27 - \theta_1}{0.0125}$$

$$\frac{dQ}{dt} = \frac{(27 - 26.48)}{0.0125} = 41.6 \text{ W}$$

**Sol 5:** In the first part of the question ( $t \leq t_1$ )

At  $t = 0$ ,  $T_x = T_0 = 400 \text{ K}$  and at  $t = t_1$ ,

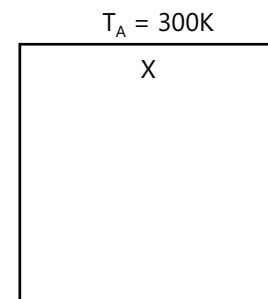
$$T_x = T_1 = 350 \text{ K}$$

Temperature of atmosphere,

$$T_A = 300 \text{ K (constant)}$$

This cools down according to Newton's law of cooling. Therefore,

rate of cooling  $\propto$  temperature difference.



$$\therefore \left( -\frac{dT}{dt} \right) = k(T - T_A)$$

$$\Rightarrow \frac{dT}{T - T_A} = -k dt$$

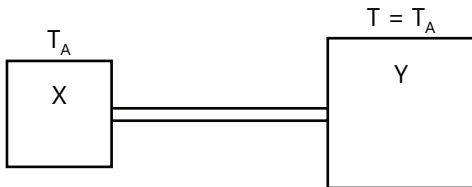
$$\Rightarrow \int_{T_0}^{T_1} \frac{dT}{T - T_A} = -k \int_0^{t_1} dt$$

$$\Rightarrow \ln\left(\frac{T_1 - T_A}{T_0 - T_A}\right) = -kt_1$$

$$\Rightarrow kt_1 = -\ln\left(\frac{350 - 300}{400 - 300}\right)$$

$$\Rightarrow kt_1 = \ln(2)$$

In the second part ( $t > t_1$ ), body X cools by radiation (according to Newton's law) as well as by conduction.



Therefore, rate of cooling

= (cooling by radiation) + (cooling by conduction)

$$\therefore \left(-\frac{dT}{dt}\right) = k(T - T_A) + \frac{KA}{CL}(T - T_A) \quad \dots (ii)$$

$$\text{In conduction, } \frac{dQ}{dt} = \frac{KA(T - T_A)}{L} = C\left(-\frac{dT}{dt}\right)$$

$$\therefore \left(-\frac{dT}{dt}\right) = \frac{KA}{LC}(T - T_A)$$

where, C = heat capacity of body X

$$\left(-\frac{dT}{dt}\right) = \left(k + \frac{KA}{CL}\right)(T - T_A) \quad \dots (iii)$$

Let at  $t = 3t_1$  temperature of X becomes  $T_2$

Then from eq. (iii)

$$\int_{T_1}^{T_2} \frac{dT}{T - T_A} = -\left(k + \frac{KA}{LC}\right) \int_{t_1}^{3t_1} dt$$

$$\begin{aligned} \ln\left(\frac{T_2 - T_A}{T_1 - T_A}\right) &= -\left(k + \frac{KA}{LC}\right)(2t_1) \\ &= -\left(2kt_1 + \frac{2KA}{LC}t_1\right) \end{aligned}$$

$$\text{or } \ln\left(\frac{T_2 - 300}{350 - 300}\right) = -2\ln(2) - \frac{2KAt_1}{LC};$$

$kt_1 = \ln(2)$  from Eq. (i)

This gives equation :-

$$T_2 = \left(300 + 12.5e^{-\frac{2KAt_1}{LC}}\right) K$$

**Sol 6:** (a) Rate of heat loss per unit area due to radiation

$$I = e\sigma(T^4 - T_0^4)$$

Here,  $T = 127 + 273 = 400 \text{ K}$

and  $T_0 = 27 + 273 = 300 \text{ K}$

$$\begin{aligned} \therefore I &= 0.6 \times \frac{17}{3} \times 10^{-8} [(400)^4 - (300)^4] \\ &= 595 \text{ W/m}^2 \end{aligned}$$

(b) Let  $\theta$  be the temperature of the oil. Then, rate of heat flow through conduction = rate of heat loss due to radiation

$$\therefore \frac{\text{temperature difference}}{\text{thermal resistance}} = (595)A$$

$$\frac{(\theta - 127)}{\left(\frac{\ell}{KA}\right)} = (595)A$$

Here, A = area of disc; K = Thermal conductivity and  $\ell$  = thickness (or length) of disc

$$\therefore (\theta - 127) \frac{K}{\ell} = 595$$

$$\therefore \theta = 595\left(\frac{\ell}{K}\right) + 127$$

$$= \frac{595 \times 10^{-2}}{0.167} + 127 = 162.6^\circ\text{C}$$

**Sol 7:** Rate of heat conduction through rod = rate of the heat lost from right end of the rod.

$$\therefore \frac{KA(T_1 - T_2)}{L} = eA\sigma(T_2^4 - T_s^4) \quad \dots (i)$$

Given that  $T_2 = T_s + \Delta T$

$$\therefore T_2^4 = (T_s + \Delta T)^4 = T_s^4 \left(1 + \frac{\Delta T}{T_s}\right)^4$$

Using binomial expansion, we have

$$T_2^4 = T_s^4 \left(1 + 4\frac{\Delta T}{T_s}\right) \quad (\text{as } \Delta T \ll T_s)$$

$$\therefore T_2^4 - T_s^4 = 4(\Delta T)(T_s^3)$$

Substituting in Eq. (i), we have

$$\frac{K(T_1 - T_s - \Delta T)}{L} = 4e\sigma T_s^3 \Delta T$$

$$\text{or } \frac{K(T_1 - T_s)}{L} = \left(4e\sigma T_s^3 + \frac{K}{L}\right) \Delta T$$

$$\therefore \Delta T = \frac{K(T_1 - T_s)}{(4\epsilon\sigma LT_s^3 + K)}$$

Comparing with the given relation,

$$\text{proportionality constant} = \frac{K}{4\epsilon\sigma LT_s^3 + K}$$

$$\text{Sol 8: } \lambda_m \propto \frac{1}{T}$$

$$\therefore \frac{\lambda_A}{\lambda_B} = \frac{T_B}{T_A} = \frac{500}{1500} = \frac{1}{3}$$

$$E \propto T^4 A$$

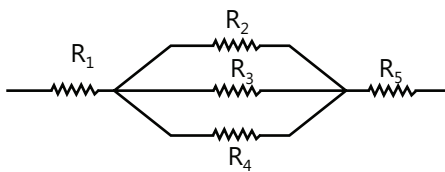
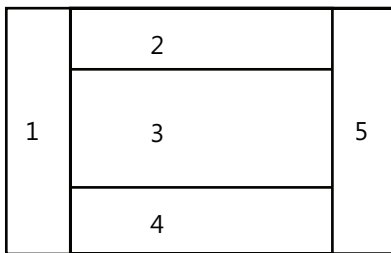
(Where A = surface area =  $4\pi R^2$ )

$$\therefore E \propto T^4 R^2$$

$$\frac{E_A}{E_B} = \left(\frac{T_A}{T_B}\right)^4 \left(\frac{R_A}{R_B}\right)^2 = (3)^4 \left(\frac{6}{18}\right)^2 = 9$$

$\therefore$  Answer is 9.

**Sol 9: (A, C, D) or (A, B, C, D)**



Let width of each rod is d

$$R_1 = \frac{1}{8kd}, R_2 = \frac{1}{3kd}$$

$$R_3 = \frac{1}{2kd}, R_4 = \frac{1}{5kd},$$

$$R_5 = \frac{1}{24kd}$$

**Sol 10: (C)**

$$\begin{aligned} \sigma A(2T)^4 + \sigma A(3T)^4 &= \sigma 2A(T')^4 & 2T & \quad \quad \quad 3T \\ 16T^4 + 81T^4 &= 2(T')^4 \\ 97T^4 &= 2(T')^4 \\ (T')^4 &= \frac{97}{2}T^4 \\ \therefore T' &= \left(\frac{97}{2}\right)^{1/4} T \end{aligned}$$

$$\text{Sol 11: (A)} \quad R_1 = \frac{L}{\kappa A} + \frac{L}{2\kappa A} = \frac{3L}{2\kappa A}$$

$$\frac{1}{R_2} = \frac{1}{\left(\frac{L}{\kappa A}\right)} + \frac{1}{\left(\frac{L}{2\kappa A}\right)} = \frac{3\kappa A}{L}$$

$$R_2 = \frac{L}{3\kappa A}$$

$$\Delta Q_1 = \Delta Q_2$$

$$\frac{\Delta T}{R_1} t_1 = \frac{\Delta T}{R_2} t_2$$

$$\Rightarrow t_2 = \frac{R_2}{R_1} t_1 = 2 \text{ sec}$$

$$\text{Sol 12: (2)} \quad \left(\frac{dQ}{dt}\right)_A = 10^4 \left(\frac{dQ}{dt}\right)_B$$

$$(400R)^2 T_A^4 = 10^4 (R^2 T_B^4)$$

$$\text{So, } 2T_A = T_B \text{ and } \frac{\lambda_A}{\lambda_B} = \frac{T_B}{T_A} = 2$$

**Sol 13: (9)** At ( $T_1 = 487 + 273 = 760\text{K}$ )  $P_1 \propto (760)^4$

i.e.  $P_1 = c(760)^4$  where c = constant

$$\log_2 \frac{P_1}{P_0} = 1 \Rightarrow P_1 = 2P_0 \Rightarrow P_0 \frac{P_1}{2}$$

at ( $T_2 = 2767 + 273 = 3040$ )

$$P_2 = c(3040)^4$$

$$\text{Reading of the sensor at } T_2 = \log_2 \left(\frac{P_2}{P_0}\right)$$

$$= \log_2 \left[2 \cdot \frac{P_2}{P_0}\right] = \log_2 \left[2 \left(\frac{3040}{760}\right)^4\right] = \log_2 [2^1 \cdot 2^8] = 9$$

$\therefore$  Reading of  $T_2 = 9$

**Sol 14: (D)**  $\Delta Q = n C_p \Delta T$ 

$$= 2 \left( \frac{f}{2} R + R \right) \Delta T = 2 \left[ \frac{3}{2} R + R \right] \times 5$$

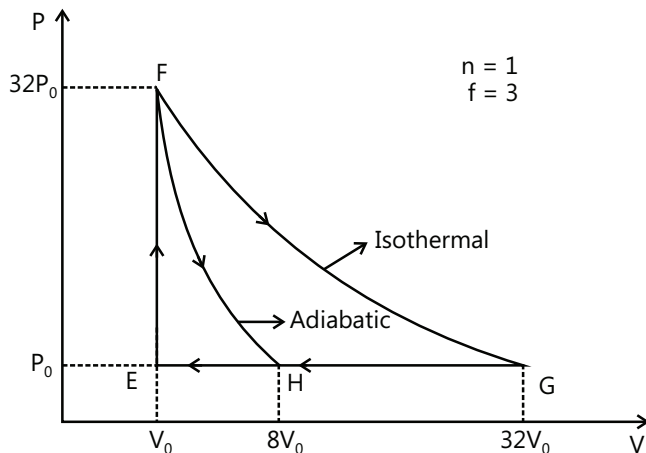
$$= 2 \times \frac{5}{2} \times 8.31 \times 5 = 208 \text{ J}$$

**Sol 15: (A)** P.  $\rightarrow$  4; Q.  $\rightarrow$  3; R.  $\rightarrow$  2; S.  $\rightarrow$  1Apply  $PV^{1+2/3} = \text{constant}$  for F to H.

$$(32P_0)V_0^{5/3} = P_0 V_H^{5/3} \Rightarrow V_H = 8V_0$$

For path FG  $PV = \text{constant}$ 

$$\Rightarrow (32P_0)V_0 = P_0 V_G \Rightarrow V_G = 32V_0$$

Work done in GE =  $31 P_0 V_0$ Work done in GH =  $24 P_0 V_0$ 

$$\text{Work done in FH} = \frac{P_H V_H - P_F V_F}{(-2/f)} = 36P_0 V_0$$

$$\text{Work done in FG} = RT \ln \left( \frac{V_G}{V_F} \right) = 160P_0 V_0 \ln 2$$

**Sol 16: (D)** 13. Heat given by lower compartment

$$= 2 \times \frac{3}{2} R \times (700 - T) \quad \dots (i)$$

Heat obtained by upper compartment

$$= 2 \times \frac{7}{2} R \times (T - 400) \quad \dots (ii)$$

equating (i) and (ii)

$$3(700 - T) = 7(T - 400)$$

$$2100 - 3T = 7T - 2800$$

$$4900 = 10T \Rightarrow T = 490 \text{ K}$$

**Sol 17: (D)** Heat given by lower compartment

$$= 2 \times \frac{5}{2} R \times (700 - T) \quad \dots (i)$$

Heat obtained by upper compartment

$$= 2 \times \frac{7}{2} R \times (T - 400) \quad \dots (ii)$$

By equating (i) and (ii)

$$5(700 - T) = 7(T - 400)$$

$$3500 - 5T = 7T - 2800$$

$$6300 = 12T$$

$$T = 525 \text{ K}$$

 $\therefore$  Work done by lower gas =  $nR\Delta T = -350 R$ Work done by upper gas =  $nR\Delta T = +250 R$ Net work done =  $100 R$